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Investigation of Prussian Blue Analogues as Cathode Materials for

Next Generation Batteries

by

Neal Walters Kuperman

# A dissertation submitted in partial fulfillment of the requirements for the degree of

Doctor of Philosophy in Applied Physics

Dissertation Committee: Raj Solanki, Chair Gary Goncher Drake Mitchell Tami Lasseter Clare Andrea Goforth

Portland State University 2020

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#### Abstract

Since the beginning of the indusial revolution, the average global temperature has risen about 1 °C due increases in anthropogenic greenhouse gases emitted into the atmosphere. Of all human produced greenhouse gases, carbon dioxide is the most prevalent, with the production of electricity from fossil fuels being the major contributor.

Solar and wind power are promising net zero emission energy sources but only accounted for ~5% of global electricity generation in 2016. The most significant hurdle hindering their widespread adoption is the intermittent nature of the electricity generation. To overcome this limitation, significant resources need to be put into the development and implementation of energy storage systems (ESS). Rechargeable batteries are one possible solution to the demand for storage, with the lithium ion battery (LIB) being the current standard. However, due to the cost, safety concerns, and toxicity of LIBs, new battery technologies are needed to fully utilize renewable energy sources, such as wind and solar.

Metal hexacyanoferrates, or Prussian blue (PB) and Prussian blue analogues (PBAs), are one family of materials whose electrochemical and physical properties make them intriguing candidates for electrode materials for non-lithium ion-based technologies. In particular, their open framework structure, high specific capacity, good ionic conductivity, facile synthesis, and tunability. The work in this dissertation examines

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four different PBAs as cathode materials in both aqueous and nonaqueous electrolytes with the aim of achieving the following objectives:

- Develop cathode materials for non-lithium ion based batteries, with a particular focus on divalent ion systems.
- 2. Determine if the physical and electrochemical storage properties of a PBA could be improved if two binary metal hexacyanoferrates are incorporated into a hybrid metal hexacyanoferrate composite.

These objectives were achieved via performing the following investigations.

In the first study, Prussian blue ( $KFe^{3+}[Fe^{2+}(CN)_6]$ ) is adopted as a cathode material for a nonaqueous calcium ion battery. The work demonstrated for the first time the use of PB in a Ca based system. The cathode delivered a specific capacity of 150 mAhg<sup>-1</sup> at a current density of 23 mAg<sup>-1</sup>.

The second study examined manganese-cobalt hexacyanoferrate in an aqueous  $Zn^{2+}$  electrolyte. The inclusion of Mn and Co in the same compound prevent the dissolution of Mn in the aqueous electrolyte. Additionally, the addition of Mn provided a 21% increase (29 mAhg<sup>-1</sup>) in storage capacity compared to CoHCF. However, the mixed metal system suffered from increased capacity loss compared to CoHCF.

The effects of coordinated and zeolitic  $H_2O$  on a  $Cu[Fe(CN)_6]$  cathode in a nonaqueous  $Mg^{2+}$  electrolyte are examined in the third study. Water was shown to play

an important role in maximizing the specific capacity of copper hexacyanoferrate. Maintaining water within the CuHCF lattice resulted in a 25% increase in specific capacity compared to the dehydrated sample. However, both samples displayed strong rate capability and exhibited comparable Mg<sup>2+</sup> diffusion coefficients.

The last experimental study presents  $Mn_xNi_{1-x}[Fe(CN)_6]$  as a cathode material in a nonaqueous K<sup>+</sup> electrolyte.  $Mn_{0.50}Ni_{0.50}[Fe(CN)_6]$  displayed superior performance compared to all other materials investigated in this work. By combing Mn and Ni, the mixed metal system was able to overcome the poor K<sup>+</sup> diffusion kinetics of Mn[Fe(CN)\_6] while delivering specific capacity 25% greater than Ni[Fe(CN)\_6].

Analysis of the FTIR and electrochemical data of Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>] suggested substitution of Mn for Ni in the PBA lattice caused a shift in electron density away from the nitrogen coordinated transition metal (either Mn or Ni) towards the Fe-C end of the cyanide. Density functional theory (DFT) calculations were performed to further study the effect of incorporation of Mn on the electronic properties of the mixed manganese-nickel hexacyanoferrate system. Initial computational results appeared to confirm the experimental hypothesis about the shifts in electron density with respect to manganese. Dedication

To my Grandmother.

Thank you for always seeing in me the person I strive be.

#### Acknowledgements

The mere fact that I have the privilege to write the acknowledgements page of my dissertation is a testament to all of the guidance, support, and comradery I have received over the past six and a half years. Countless people within the Portland State University community, especially in the physics department, have contributed to my growth and development as a learner, thinker, and researcher, and I want to acknowledge a few people in particular.

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#### Chapter 1.

#### Introduction

## 1.1 Global Warming and Electricity Production

Eighty-four countries signed the Kyoto protocol in 1992 [1], signaling a worldwide acknowledgment that human production of greenhouse gases (GHG) had caused the average temperature of the Earth to increase about 1 °C since the beginning of the industrial revolution in 1763. Since 1992 an additional 107 countries have joined the Kyoto agreement and climate change has been widely accepted as one of the largest existential threats to the global community. Nevertheless, greenhouse gas emissions have continued to rise and nine of the hottest years on record, dating to 1880, have occurred since 2005 [2].

The relationship between climate change and greenhouse gases is well understood. When visible and ultraviolet (UV) radiation from the sun reach the Earth, 30% is reflected back into space, 23% is absorbed by particles in the atmosphere, and 47% is absorbed by land and ocean [3]. Much of the energy absorbed by land and ocean water is re-radiated back into the atmosphere as infrared (IR) radiation, i.e. heat. Greenhouse gas molecules in the atmosphere, although transparent to the sun's visible and UV radiation, absorb significant amounts of the IR radiation emanating from the Earth's surface. Greenhouse gases absorb IR radiation through excitation of stretching and bending modes of molecular bonds. Absorbed IR light is re-emitted in all directions, with about half escaping into outer space and the other half being directed back down to the earth's surface, resulting in warming of the Earth and lower atmosphere. This warming of the Earth through absorption and remission of IR light is called the greenhouse effect.

Naturally occurring greenhouse gases in the atmosphere include water vapor,  $CO_2$ , methane (CH<sub>4</sub>), and nitrous oxide (N<sub>2</sub>O). These gases maintain the Earth at a temperature about 35 °C higher than it would be if these gases were not present, i.e. 14 °C rather than -21 °C [4,5]. The most important of the greenhouse gases is  $CO_2$ , due to its relative abundance in the upper regions of the atmosphere. Between ~800,000 BCE and 1763 CE, atmospheric  $CO_2$  levels fluctuated within a relatively narrow range, between 173 and 299 ppm [6].

In contrast, since the start of the industrial revolution in 1763, average atmospheric CO<sub>2</sub> concentrations have risen to 320 ppm, with a peak of 408 ppm in 2018 [7]. This increase in CO<sub>2</sub> is attributed to the combustion of fossil fuels as energy sources, the production of cement, and deforestation with an associated decrease in photosynthesis. Additionally, man-made GHGs such as hydrofluorocarbons (HFCs), perfluorocarbons (PFCs), and sulfur hexafluoride (SF<sub>6</sub>) have been introduced into the environment.

2

In addition to global warming, increased GHG emissions are having other negative climatic effects including increased ocean acidity, eradication of ecosystems and increased glacier melting [8]. In 2018 the United Nations' international Panel on Climate Change (IPCC) warned that if the increase, from pre-industrial values, in average global temperature exceeds 1.5 °C by 2050, considerable and potentially irreversible damage to the environment and humanity will become inevitable [2,3]. With their warning, the IPCC also set out goals and emission targets, specifically calling for a "fundamental transformation of the energy supply system" to stave off a climatic catastrophe [9].

The production of electricity from fossil fuels is a major contributor to atmospheric CO<sub>2</sub> and accounted for 32% of all man-made CO<sub>2</sub> emissions in 2016 [9]. To dramatically decrease the emissions of the energy supply sector, which includes energy extraction, conversion, storage, transmission, and distribution processes, a radical shift in how we produce and consume energy is needed. One key piece in any energy solution will be a major growth in electricity production from sources that produce little or no atmospheric CO<sub>2</sub>.

The main energy sources used to produce electricity with minimal or no CO<sub>2</sub> production are nuclear, hydroelectric (water), solar, wind and geothermal. These sources cause much less CO<sub>2</sub> production than the combustion of fossil fuels, even when one accounts for the CO<sub>2</sub> produced during the manufacturing and distribution of the equipment needed for ongoing electricity generation.

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Solar and wind power accounted for only ~9% of global electricity generation in 2020, in spite of their favorable  $CO_2$  footprint [10]. The most significant hurdle hindering the widespread adoption of solar and wind is the intermittent nature of the electricity generation. To overcome this limitation, significant resources need to be put into the development and implementation of energy storage systems (ESS).

### 1.2 Energy Storage Systems

There are numerous methods to store energy, each with its own set of benefits and weaknesses. When comparing the different available storage technologies for a particular application or community, some of the key considerations are:

- The amount of energy that can be stored per unit volume or unit mass (energy density),
- 2. The power that can be delivered per unit volume or unit mass (power density),
- 3. The energy efficiency,
- 4. The lifetime, and
- 5. How long the energy can be stored without significant loss, i.e. self-discharge.

For example, if a particular application requires that energy be delivered sparsely over long durations, then a storage system with high energy density would be desirable. However, if large amounts of energy are required quickly, then power density is the most important factor.

### **1.2.1** Pumped Hydro energy storage

Pumped hydro storage (PHS) systems store energy in the form of gravitational potential energy by moving water between a low elevation reservoir and a high elevation reservoir. PHS is typically charged during times of low energy demand and low costs, and discharged during high cost and high demand times. As of 2020, PHS accounts for 95% of all deployed energy storage systems in the world [11]. The main benefit of pumped hydro is its very low self-discharge rate, allowing energy to be stored for long periods of time. However, low energy density, high upfront capital costs and geographic limitations restrict the construction of new pumped hydro systems.

#### **1.2.2** Thermal energy storage

Thermal energy storage (TES) systems store energy in the form of heat. Common materials used in TES systems include rocks, concrete, water, and salts. The heat stored can be generated naturally, e.g. heating water with sunlight, or can be man-made, e.g. waste heat from industrial processes. TES is categorized into three systems depending on the way heat is stored: sensible, latent, and thermochemical systems.

Sensible heat storage is the oldest and most common form of TES, in which thermal energy is stored by raising the temperature of the storage medium. The amount of energy stored is described by Equation 1.1.

5

$$q = mC_p(T_H - T_C) \tag{1.1}$$

where q is the heat stored (J), m is the mass of the material storing the heat (kg),  $C_p$  is the material's specific heat at constant pressure (J kg<sup>-1</sup>K<sup>-1</sup>), and T<sub>H</sub> and T<sub>C</sub> are the hot and cold temperatures (K).

Latent heat storage capitalizes on the energy required to induce a phase change in a material. Phase changes occur at constant temperatures in the material of interest, absorbing heat during solid  $\rightarrow$  liquid or liquid  $\rightarrow$  gas transitions, and releasing heat during the opposite transitions. The equation for latent heat for a solid to liquid phase change at the melting point is given in equation 1.2.

$$q = mL \tag{1.2}$$

where q is heat (J), m is the mass (kg) of the material undergoing the phase change and L is the latent heat of fusion (J kg<sup>-1</sup>).

The last form of thermal storage is thermochemical storage, in which energy is stored in a reversible endothermic chemical reaction. Some examples include magnesium sulfate/water, calcium sulfate/water, calcium hydroxide/water and iron oxide (FeO)/carbon dioxide [12]. The major benefits of thermochemical storage are its ability to be implemented in a wide variety of settings, and store energy with minimal loss over long periods of time. Each of the thermal energy storage technologies has drawbacks. Sensible and latent heat storage both have slow discharge times, limiting the power output, while thermochemical is a nascent technology that is currently cost prohibitive.

#### **1.2.3** Mechanical energy storage

Mechanical energy storage systems convert electrical energy into either mechanical potential energy or kinetic energy. Two examples are the flywheel and compressed air energy storage.

A flywheel is an electromechanical device that uses a motor to rotate a wheel to very high speeds. The energy stored is given by equation 1.3.

$$E_{kinetic} = I\omega^2 \tag{1.3}$$

where  $E_{kinetic}$  is rotational kinetic energy, I is the moment of inertia of the rotating object and  $\omega$  is its angular velocity. Flywheel technology is still not mature enough for mass deployment, but is theoretically suitable for high power applications.

Compressed air energy storage technology (CAES) stores energy in the elastic potential energy of a compressed gas. CAES systems typically use off-peak, low cost energy to compress a gas in underground caverns or in above-ground mechanical tanks. Energy is recovered when the stored, high pressure gas is used to drive a turbinegenerator. Low energy efficiency, around 70%, is a major drawback to compressed air storage.

#### 1.2.4 Hydrogen storage

Energy can be stored through the production of  $H_2$  by electrolysis, as shown in the reaction that follows.

$$2H_2O(aq) + 2e^- \to H_2(g) + 2OH^-(aq)$$
 (1.4)

There are numerous different ways to store the hydrogen gas once it is produced, including as a compressed gas, as liquid hydrogen (stored at -253 C), absorbed within a solid or stored in an alternative chemical bond. Energy can be reclaimed, as electricity, by oxidizing the hydrogen gas, such as occurs in the reaction between O<sub>2</sub> and H<sub>2</sub> in a fuel cell. Hydrogen energy storage has the highest theoretical energy density of the storage methods discussed [13]. However, problems with loss of hydrogen gas during storage, low efficiency and safety concerns currently limit adoption of this method. Most notable, the round trip efficiency of current hydrogen storage technology is on the order of 35% [14,15]

#### **1.2.5 Electrochemical capacitors**

Conventional parallel plate capacitors, which store energy in the electric field between two oppositely charged species some distance *d* away from each other, are of very limited use as large scale energy storage systems due to their low energy densities. This limitation spurred the development of higher energy density electrochemical doublelayer capacitors (EDLC), in which the electrostatic interactions occur at the electrode/electrolyte interface between adsorbed charged species in the electrolyte and

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the conducting electrodes (Figure 1.1). The region of ion accumulation is known as the Helmholtz layer. The simplest estimation of the capacitance of an EDLC is given by

$$C = \frac{Q}{V} = \frac{\epsilon_0 \epsilon_r A}{d} \tag{1.5}$$

where C is the capacitance, Q is the charge stored, V is the potential between an electrode and the charged ions,  $\varepsilon_0$  is the dielectric constant of vacuum,  $\varepsilon_r$  is the dielectric constant of the electrolyte, A is the electrode-electrolyte surface area, and d is the charge separation distance. The energy stored in an EDCL with a capacitance C that can be estimated by

$$U = \frac{1}{2}CV^2 \tag{1.6}$$

where U is the energy stored in the capacitor, and C and V are as previously defined. EDLCs have extremely fast charge and discharge rates, making them desirable for highpower applications. However, EDCLs suffer from high self-discharge rates and their



Figure 1.1 Schematic of a charge electrochemical double layer capacitor

energy density is much lower than other non-capacitor technologies, making them unsuitable for long term energy storage.

#### **1.2.6** Pseudocapacitors

Pseudocapacitors are a hybrid between traditional batteries and EDCLs. The majority of charge storage occurs through reversible charge transfer reactions at the electrode/electrolyte interface, with some additional storage in an electrochemical double-layer. Because the reactions take place entirely at the surface of the electrode, pseudocapacitors offer charge and discharge rates much higher than batteries. However, because they do not utilize the entire volume of a material, the energy density of pseudocapacitors is relatively low.

## 1.2.7 Batteries

Batteries interconvert electrical energy and chemical energy through electrochemical redox reactions. Compared to other electrochemical storage systems, batteries offer high energy densities and relatively low power densities. However, the power density of modern batteries is high enough to make them suitable for a wide range of applications, ranging from powering portable electronics to storing gigawatts of wind and solar energy. Under the umbrella of battery technologies, there are two overarching groups: flow batteries and solid electrode batteries.

Flow batteries allow for the decoupling of power and storage capacity, unlike other electrochemical storage systems. Electrolytes, representing stored chemical energy, are housed in large external tanks and are pumped into cell stacks when electricity needs to be generated. Storage capacity can be increased by increasing the size of the tanks or the concentrations of reactive redox species. Total power output can be modulated by adjusting the number of stacks or changing the electrolyte flow rate. Some of the most promising flow battery chemistries are based on all-iron, all-vanadium, ironchromium mixtures and zinc-bromine mixtures. The major drawbacks to flow batteries are low energy density, high self-discharge rates, and system stability.

A solid electrode battery is a completely closed system with an anode, cathode and electrolyte all in the same cell. During charging and discharging, positively charged ions in the electrolyte migrate back and forth between the anode and cathode, where oxidation and reduction reactions occur. Mirroring the flow of ions through the electrolyte, electrons are transferred through an external circuit to maintain charge balance. Energy capacity is dependent on the total amount of redox active species in the electrodes; the electrolyte acts solely as a transport medium for charged ions.

By utilizing the entire volume of an electrode material, solid electrode batteries have high energy densities, making them suitable for a wide range of applications. However, difficulties delivering high voltages and currents prevent solid electrode batteries from being used in applications that require rapid charge-discharge cycling or very high power. Despite their limitations, the mix of high energy density, scalability, and stability make solid electrode batteries one of the most promising technologies for long term energy storage.

#### 1.3 Solid Electrode Batteries as an Energy Storage Solution

### **1.3.1 Primary Batteries**

A primary (non-rechargeable) battery is an electrochemical cell designed for single use without the ability to be recharged. The first primary battery was discovered in 1799 by the Italian physicist Alessandro Volta. By stacking alternating copper and zinc plates separated by paper discs soaked in salt water, Volta realized that an electrical current could be generated that was proportional to the number of metal plates [16]. The half reactions for Volta's battery, aptly named the Voltaic pile, are shown in equations 1.7 and 1.8.

$$Zn^0(s) \to Zn^{2+}(aq) + 2e^-$$
 (1.7)

$$2H^{+}(aq) + 2e^{-} \rightarrow H_{2}(g)$$
 (1.8)

The copper plates did not participate in the electrochemical reaction, and acted only as a current collector. Batteries based on Volta's work were the predominant source of electricity for nearly 70 years until the dynamo, an electric generator, was introduced into the electricity industry.

#### **1.3.2 Secondary Batteries**

60 years after the invention of the Voltaic pile, French physicist Gaston Planté revolutionized the energy world by inventing the first secondary (rechargeable) battery. The lead acid battery, as constructed by Planté, consisted of two rolled sheets of lead separated by rubber and submerged in 10% sulfuric acid. Each lead acid cell provides nearly 2 V. The positive and negative plate half reactions, and the full-cell discharge reaction are shown in equations 1.9 - 1.11, respectively:

$$Pb^{4+}O_2 + HSO_4^- + 3H^+ + 2e^- \to Pb^{2+}SO_4 + 2H_2O$$
(1.9)

$$Pb^{0} + HSO_{4}^{-} \to Pb^{2+}SO_{4} + H^{+} + 2e^{-}$$
 (1.10)

$$Pb^{4+}O_2 + Pb^0 + 2H_2SO_4 \to Pb^{2+}SO_4 + 2H_2O$$
(1.11)

To charge the battery, a potential is applied to promote the reverse reactions. Because of the long lifetime, good power, and stability, the lead acid battery is still widely used across numerous industries.

# **1.3.3 Lithium Ion batteries**

Secondary lithium ion batteries (LIBs) have become the primary battery technology due to their relatively high energy density, good cycle lifetime and ability to be scaled to meet the needs of a specific application. LIBs were first invented in the 1970s

by Dr. Michael Whittingham, but did not become a reliable energy storage option until 1985. It was the work of Dr. John Goodenough in 1980, who first demonstrated layered LiCoO<sub>2</sub> as an intercalation cathode [17], and Dr. Akira Yoshino in 1985, who developed a safe and energy dense graphitic carbon anode [18], that introduced the world to the modern LIB. Since commercialization in 1991 by Sony, LIB research has largely focused on the discovery of new cathode materials, as the cathode is the bottleneck to increased energy density.

LIB cathodes are categorized as either conversion or intercalation electrodes, depending on the chemistry underlying the storage of Li ions. Conversion electrodes store energy by breaking and creating chemical bonds during the insertion and extraction of Li ions. The high theoretical energy densities of conversion reaction cathodes, such as Li<sub>2</sub>O<sub>2</sub> and Li<sub>2</sub>S, have made them of great interest. However, problems such as large structural expansions during charging and discharging, and dissolution of the active material have made them unusable in a commercial battery.

Intercalation electrodes charge and discharge as Li<sup>+</sup> ions migrate through the interstitial spacing of the host lattice, occupying vacancies while transition metals in the electrode undergo oxidation and reduction. Three classes of materials have garnered the most interest as intercalation cathodes for LIBs: layered transition metal oxides, spinel transition metal oxides, and polyanion oxides.

## 1.3.3.1 Layered Transition Metal Oxides

Layered transition metal oxides (LTMO) with the general formula LiMO<sub>2</sub> (M = transition metal) crystallize in a rock salt structure with alternating layers of the sequence O-Li-O-M-O (Figure 1.2). Insertion/extraction of Li ions occur between the covalently bonded MO<sub>2</sub> layers. The crystallographic configuration of LTMOs allows for fast two-dimensional ionic migration. The lithium pillars between the MO<sub>2</sub> layers are integral to the integrity of the rock salt layered structure. For LiCoO<sub>2</sub>, the original LIB cathode and an example of a LMTO, the structural Li ions will de-intercalate upon charging above 4.2V, resulting in a phase transition and degradation of the material. This limits the operating potential of LMTOs, and thus the potential of the overall battery cell.



Figure 1.2. Crystal structure of layered LiCoO<sub>2</sub> [19,20]

## 1.3.3.2 Spinel Transition Metal Oxides:

Spinel transition metal oxides (STMO) possess the general formula  $LiM_2O_4$  (M = transition metal) and crystalize in a tetragonal spinel structure with space group Fd3-m where the Li and M are tetrahedrally and octahedrally coordinated to the oxygen, respectively. The  $[M_2]O_4$  edge-shared octahedrons form intercalation/deintercalation pathways for Li ions.  $LiMn_2O_4$  was the first STMO studied and displays a two-step intercalation/deintercalation process at 4 V and 3 V (vs Li/Li<sup>+</sup>). Figure 1.3 shows the crystal structure for  $LiMn_2O_4$ . The redox reaction at 3 V induces a cubic to tetragonal phase shift and causes structural instabilities. Because of this only the redox reaction at 4 V can be utilized effectively, eliminating half of the storage capacity of  $LiMn_2O_4$ . Further problems



Figure 1.3 Crystal structure of spinel LiMn<sub>2</sub>O<sub>4</sub> [20,21]

occur from the dissolution of Mn during operation. Mixed metal STMOs (LiMn<sub>2</sub>-xMxO<sub>4</sub>) have been studied with the hope of overcoming the Mn dissolution. Although Mn dissolution can be suppressed, the substitution of other metals for Mn increases the operating potential of the LiMn<sub>2</sub>-xMxO<sub>4</sub>, making them unusable with current nonaqueous electrolytes.

# 1.3.3.3 Polyanion Oxides

Polyanion oxides of type  $LiM_{y}(XO_{4})_{n}$  (X = S, Mo, P, and W; and M = transition metal) were first investigated in an effort to find a set of transition metal oxides that were stable during Li intercalation/deintercalation [22–27]. The materials crystallize in the



Figure 1.4 Crystal structure of olivine LiFePO<sub>4</sub> [20,29]
orthorhombic olivine structure with space group Pnma (Figure 1.4) [28]. The goal of replacing the oxygen with a polyanion was to utilize lower-valent transition metals to suppress the structural distortions observed with  $LiCoO_2$  ( $Co^{3+/4+}$ ) and  $LiMn_2O_4$  ( $Mn^{3+/4+}$ ).  $LiFePO_4$  ( $Fe^{2+/3+}$ ) was shown to successfully undergo charge/discharge cycling with Li ions. By replacing O with PO, the  $Fe^{2+/3+}$  redox potential could be elevated from 2.5 V vs  $Li/Li^+$  (for  $Fe_2O_3$ ) to 4.1 V vs  $Li/Li^+$  (for  $LiFePO_4$ ). The challenge of polyanion oxides, and  $LiFePO_4$  in particular, is their poor performance at high currents. This limits the power density and limits high charging/discharging capacities to low current densities.

### **1.3.4 Moving Beyond Lithium Ion Batteries**

Despite their widespread adoption, lithium ion batteries have significant limitations with regards to cost, safety, and toxicity, restricting their potential for grid scale storage. New lithium chemistries such as lithium-air [30–36] and lithium-sulfur [37–40] are being explored due to their high energy densities, however neither have been shown to be stable or offer lifetimes greater than a few charge/discharge cycles. The mass deployment of any lithium ion storage technology is further constrained by the scarcity of lithium salts in the Earth's crust (1.6x10<sup>7</sup> tons, 20 ppm) [41]. To meet the storage needs of intermittent solar and wind powered electricity production, novel, low cost, storage solutions must be designed that prioritize the use of non-toxic, safe, and abundant materials while maintaining long lifetimes.

In recent years, battery chemistries based on abundant elements such as sodium [42–49], potassium [50–56], magnesium [57–63], calcium [56,64–70], or aluminum [71– 76] have emerged as low-cost alternatives to LIBs. Attempts to transition cathodes from lithium ion batteries to alternate systems has proven difficult. The relatively narrow interstitial pathways of the cathodes that worked well with lithium ion have prohibitively slow diffusion with larger or more highly charged ions that are present in non-lithium systems [77]. Thus, developing alternative cathode materials is paramount to the success of non-lithium ion technology. One class of materials that has garnered a lot of attention is Prussian blue analogues (PBAs).

#### 1.4 Prussian Blue (PB) and its Analogues (PBAs)

Iron hexacyanoferrate, also known as Prussian blue, was first discovered in 1704 by the German colormaker Diebach of Berlin while attempting to make a crimson paint [78]. By happenstance, Diebach combined "animal oil", a distillation of animal blood that unknowingly contained cyanide, with a solution of iron sulfate and produced Prussian blue [79]. Between 1704 and 1977, Prussian blue was used in numerous applications ranging from early photocopying to gas purification. It was not until the work of Vernon Neff in 1978 that the electrochemical properties of Prussian blue were first explored [80]. Since Neff, Prussian blue and its analogues (PBAs) have continued to provide promising results in the search for cathode materials for secondary batteries, due to several properties that are desirable for energy storage: large interstitial pathways, high specific capacity, good ionic conductivity, facile synthesis and tunability.

#### 1.4.1 Prussian Blue and Prussian Blue Analogues Chemical Composition

#### 1.4.1.1 Prussian blue

Prussian blue is a mixed valence coordination compound with the general chemical formula AFe<sup>3+</sup>[Fe<sup>2+</sup>(CN)<sub>6</sub>], where A is a monovalent alkali cation, (CN) is the cyanide anion, low spin (LS) Fe<sup>2+</sup> is coordinated to C, and high spin (HS) Fe<sup>3+</sup> is coordinated to cyanide N. The PB framework consists of (C=N)<sup>-</sup> anions bridging the FeN<sub>6</sub> and FeC<sub>6</sub> octahedra, which form a face-centered cubic structure with space group Fm3m and a lattice parameter of 10.2 Å [81]. The open framework of PB allows for the reversible intercalation of a large variety of monovalent and multivalent cations, including Na<sup>+</sup> [47,49,55,82–97], K<sup>+</sup> [98–109], Mg<sup>2+</sup> [110–115], Ca<sup>2+</sup> [56,66,87,113,116,117], Zn<sup>2+</sup> [118–122] and Al<sup>3+</sup> [71,72,123,124]. Charging and discharging of PB is a two-step process as shown in

Figure **1.5**, with the C-coordinated Fe and N-coordinated Fe undergoing redox at different potentials. This asymmetry arises from differences in the ligand field strengths at opposite ends of the cyanide, causing the high-spin (HS) FeN6 octahedra and low-spin (LS) FeC6 octahedra.



**Figure 1.5** Schematic depiction of charge and discharge mechanisms of Prussian blue.

## 1.4.1.2 Prussian Blue Analogues

Prussian blue analogues (PBAs) are a class of mixed valence compounds that result from the substitution of a transition metal in place of one or both of the coordinated irons in PB. PBAs have the general formula

$$A_xM'_a[M(CN)_6]_y \cdot \Box_{1-y} \cdot nH_2O$$

where A is an alkali cation, M' is the N-coordinated transition metal; M is the C-coordinated transition metal,  $M(CN)_6$  is the hexacyanometallate anion,  $\Box$  is a  $[M'(CN)_6]^{3/4-}$  vacancy, and 0 < x < 2; 0 < y < 1. Water molecules can be present in two unique crystallographic environments: either coordinated to unbonded M' atoms

(coordinated water), or residing in interstitial spacing of the crystal (zeolitic water) [81,125–127]. The substitution of different metals into the PB framework creates a large family of materials with varying physical and crystallographic properties that affect electrochemical properties.

#### 1.4.1.3 Lattice Vacancies and Structural Water in PBAs

Hexacyanometallate vacancies, as well as both coordinated and zeolitic water, have been shown to play integral roles in the electrochemical properties of a PBA, with both disadvantageous and advantageous effects.

#### **Disadvantageous Effects of Vacancies and Water**

One of the most important properties of a battery is total energy storage. Specific capacity (mAhg<sup>-1</sup>) is a measure of the capacity, or energy stored, per unit weight. Early PBA cathodes failed to deliver specific capacities above 100 mAhg<sup>-1</sup> despite high theoretical capacities of ~170 mAhg<sup>-1</sup> [128,129]. Cathodes of Mn<sup>2+</sup>, Fe<sup>2+</sup>, Co<sup>2+</sup>, Ni<sup>2+</sup>, Cu<sup>2+</sup> or Zn<sup>2+</sup> PBAs, synthesized via co-precipitation, experienced poor coulombic efficiencies and a maximum reversible capacity of 70 mAhg<sup>-1</sup> [128]. These low values were thought to be due to structural instabilities and side reactions caused by lattice vacancies and coordinated water molecules introduced during synthesis [130–135]. Vacancies can also cause low specific capacities, as missing redox active hexacyanometallate anions are replaced by water molecules. Thus, numerous studies have tried to eliminate defects and

control the coordinated water content through novel synthesis procedures [131,132,136–138].

In order to limit the formation of defects, a single precursor synthesis has been proposed, where PB is synthesized from ferrocyanide in an acid solution [134,138,139]. High quality PB (HQ-PB) particles were produced using this method, and compared with low quality PB (LQ-PB) synthesized under the unmodified co-precipitation technique [134]. Although the structures of the HQ-PB and LQ-PB were identical, they had 6% and 32% vacancies by weight, and 15% and 20% water content by weight, respectively. By limiting defects and reducing coordinated water, the HQ–PB exhibited superior electrochemical properties with a high specific capacity (170 mAhg<sup>-1</sup>), no apparent capacity loss over 150 cycles and a coulombic efficiency near 100% .

Wu et al. produced a low vacancy NaCo[Fe(CN)<sub>6</sub>] through a citrate-assisted synthesis [130]. With the addition of trisodium citrate as a chelating agent, the reaction rate and crystallization process were slowed, allowing for a more controlled growth. The resulting material showed reductions in lattice defects and water content of 11% and 52% respectively when compared to a control synthesized without citrate ions. The pristine NaCo[Fe(CN)<sub>6</sub>] displayed a higher specific capacity (150 mAhg<sup>-1</sup>) than the control (115 mAhg<sup>-1</sup>), attributed to suppressed defects and coordinated lattice water. Other reports of citrate-assisted synthesis have also delivered high capacities and lifetimes [130,140–145].

In addition to the above procedures, other methods to reduce the water content of PBAs have been proposed including synthesis of carbon/PB composites [131,136,146,147] mixed solution synthesis [148], and annealing as-synthesized PBAs at elevated temperatures [149]. All of these techniques have resulted in increased capacity and cathode lifetime, highlighting the importance of synthetic conditions.

#### Advantageous Effects of Vacancies and Water

Whereas the above studies demonstrated undesirable electrochemical effects of hexacyanometallate vacancies and coordinated or zeolitic water, other studies have demonstrated that these effects are not strictly negative. For aqueous electrolytes, water offers charge screening between the lattice and the intercalating ions, which allows for high ionic mobilities on the order of 10<sup>-7</sup> cm<sup>2</sup> s<sup>-1</sup> [150]. Additionally, zeolitic and nitrogen coordinated water can facilitate the migration of ions in PBAs [87]. Padigi et al. and others have demonstrated the use of hybrid aqueous/nonaqueous electrolytes can lead to improved electrochemical performances and increase specific capacities by more than 45% [65,151–153]. Xiao et al. carried out a theoretical study on the impacts of structural and zeolitic water to Na<sub>2</sub>FeMn(CN)<sub>6</sub>, proposing water caused a phase change and an increase in redox potentials [154]

#### **1.4.1.4 Crystal Structure of PBAs**

The crystal structures of PBAs have been shown to affect their energy storage capacities. Recently, rhombohedral PBAs have become of interest, displaying superior

performance when compared to their cubic counterparts [47–49,130,134,141]. Wang et al. determined that the induced phase change for Mn[Fe(CN)<sub>6</sub>] occurred with increased Na<sup>+</sup> ions in the lattice [48]. Although the rhombohedral and cubic Mn[Fe(CN)<sub>6</sub>] have similar discharge capacities, the rhombohedral phase has a higher operating voltage and thus higher energy density. A similar effect on the operating voltage of Ni[Fe(CN)<sub>6</sub>] was observed, where the cubic and rhombohedral materials had a 120 mV offset in operating potential [141]. It was proposed that in the rhombohedral structure, the intercalated sodium atoms caused a dramatic polarization of the electron density in the crystal lattice away from the Ni-N bond towards the Fe-C bond. This polarization in turn raised the redox potential of the iron in the rhombohedral nickel hexacyanoferrate.

In addition to the effect of the microcrystalline structure of a PBA on its battery performance, the macro structure plays an important role in a material's electrochemical properties. Zhang et al. synthesized rhombohedral cuboctahedron (C-RZnHCF), truncated octahedron (T-RZnHCF), octahedron (O-RZnHCF) and Zn[Fe(CN)6] nanostructures by varying the rate of mixing of the reactants during synthesis [122]. Each material crystallized with the same phase and lattice parameter, but displayed different macroscopic geometries (Figure 1.6). The initial specific capacities were the same for each sample, however after 100 cycles at 300 mAg<sup>-1</sup> C-RZnHCF maintained a higher percentage of its initial capacity than the other two materials. By adjusting the macro and micro crystallographic properties of a PBA, the electrochemical properties of the materials can be improved.



**Figure 1.6** Zn[Fe(CN)6] nanostructures with different macroscopic geometries (a) Rhombohedral cuboctahedron (C-RZnHCF), (b) truncated octahedron (T-RZnHCF), and (c) octahedron (O-RZnHCF) [117]

## **1.4.1.5 PBA Crystal Redox Active Elements**

To maximize the theoretical capacity of a PBA, both C-coordinated and Ncoordinated transition metals must be redox active. However, when PBAs such as Fe[Fe(CN)<sub>6</sub>], Mn[Fe(CN)<sub>6</sub>] and Co[Fe(CN)<sub>6</sub>] undergo redox, the lattice expands and contracts, which may result in structural deterioration [155]. This in turn causes the capacity to quickly fade. By introducing a non-redox active element, it is possible to reduce the stress and strain on the lattice and improve stability over time. You et al. reported on Ni[Fe(CN)6] as a zero-strain insertion cathode, where Ni did not undergo redox [156]. Under the insertion and extraction of Na ions, the change in lattice parameters was less than 1%. This structural stability was associated with a capacity retention of 99.7% over 200 cycles and a coulombic efficiency of 100%. Theoretical calculations were performed for NiHCF, in which the volume variation for Na<sup>+</sup> intercalation was predicted to be 0.72% [141].

#### 1.4.1.6 Mixed Metal Hexacyanoferrates (MMHCFs)

The electrochemical and physical properties of PBAs are distinct from PB due to effects arising from the different transition metals that are present in PBAs. Additional variations in properties can be induced by partially substituting a third metal atom into a PBA, resulting in a mixed-metal, or ternary, hexacyanometallate. Maintaining the ferrocyanide anion and varying the nitrogen coordinated metal results in a mixed-metal hexacyanoferrate with the chemical formula

## $A_xM'_{1-z}M''_z[M(CN)_6]_y \cdot \Box_{1-y} \cdot nH_2O$

where M is Fe, and M' and M'' are two different nitrogen bonded transition metals. By varying the ratio of M' to M'', it becomes possible to tune specific properties of a PBA. This feature of MMHCFs has been utilized in areas such chemical sensing [157–160], magnetic materials [161–164], and catalysis [165–169]. The application of ternary hexacyanoferrates to energy storage has mainly focused on sodium ion batteries [83,91,96,97,150,170–174], with minimal reports on other chemistries [71,100,107,175–178].

Bharathi et al. investigated the redox behavior of mixed metal hexacyanoferrates by substituting Ni or Mn for some of the Fe in PB [179]. In the study, the three binary systems (Mn[Fe(CN)<sub>6</sub>], Ni[Fe(CN)<sub>6</sub>] and Fe[Fe(CN)<sub>6</sub>] were compared to the mixed metal hexacyanoferrates (MnFe[Fe(CN)<sub>6</sub>] and NiFe[Fe(CN)<sub>6</sub>]). Differences in the redox properties between the two binary parent systems and the tertiary mixed metals were

observed. Most interestingly, while Mn[Fe(CN)]<sub>6</sub> was unstable the incorporation of Mn into the PB lattice stabilized the Mn-C-N-Fe chain. However, a critical concentration of Mn was identified where increased Mn led to dissolution of the material.

The electrodeposited materials studied by Bharathi et al. did not allow for crystal analysis due to the limited amount of product produced. XRD analysis was possible on the Fe<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>] system, synthesized in sufficient quantities via coprecipitation [180]. A linear relationship between the materials' lattice constants and the percentage of nickel was observed. The authors proposed the formation of a single mixed phase, as only one voltammetric response was observed instead of the two systems present when both binary HCFs were mixed together.

The first comprehensive investigation into the structural properties of mixed metal hexacyanoferrates was performed for  $Fe^{3+}Cd^{2+}[Fe(CN)_6]$  by varying the  $Cd^{2+}$ concentration [181]. It was discovered that for products with a molar ratio  $m_{Cd} = n_{Cd}/(n_{Cd} + n_{Fe})$  less than 0.126, Cd only resided in the interstitial space of the Prussian blue lattice. For samples with  $m_{Cd} \le 0.4$ , the cubic phase of PB was maintained with partial  $Fe^{2+}$  replaced by  $Cd^{2+}$ , whereas those with higher ratios underwent a phase change to an orthorhombic structure. Coinciding with the phase transition from cubic to orthorhombic, a partial oxidation of the low-spin irons occurred.

The transition energies, or band gap energies, of the nickel iron  $Fe_xNi_{3-x}[Fe(CN)_6]_2$ system were studied by Ishizaki et al. [182]. It was reported that the color of the solid

precipitants gradually changed from blue to yellow with increasing Ni concentration. Employing vis-near-IR absorption spectra, a linear correlation between composition ratio (0.6< x< 3.0) and a material's absorption was identified. The transition energies were estimated to be 1.44 eV (x=3), 1.36 eV (x=2.4), 1.27 eV (x=1.5) and 1.2 eV (x=0.6). Although Ni has been shown to be redox inactive in PBAs [156,183,184], a linear shift in potential between 0.58 V and 0.87 V for the first redox couple (Fe<sup>2+</sup>/Fe<sup>3+</sup>) was observed with increasing Ni concentration. The authors showed that the energy levels of Fe<sub>x</sub>Ni<sub>3-x</sub>[Fe(CN)<sub>6</sub>]<sub>2</sub> could be systematically tuned by adjusting the Ni concentration.

As briefly highlighted above, the addition of a third transition metal into the PBA lattice leads to novel structural, chemical, and electrical properties that can be tuned based on the material's composition. Table 1.1 provides a different published mixed metal hexacyanoferrate systems that have been investigated for electrochemical energy applications.

Material	Intercalating ion	Ref	
NiCo[Fe(CN) <sub>6</sub> ]	К	[100,185–187]	
NiCo[Fe(CN) <sub>6</sub> ]	Na	[83,91,188,189]	
MnCu[Fe(CN) <sub>6</sub> ]	Li	[190]	
MnCo[Fe(CN) <sub>6</sub> ]	Li	[191]	
MnCo[Fe(CN) <sub>6</sub> ]	К	[192]	
MnCo[Fe(CN) <sub>6</sub> ]	Na	[150,153,192,193]	
CuNi[Fe(CN) <sub>6</sub> ]	Na	[97,170]	
(VO)Cu[Fe(CN) <sub>6</sub> ]	Li	[149]	
FeNi[Fe(CN) <sub>6</sub> ]	Na	[172,194,195]	
FeNi[Fe(CN) <sub>6</sub> ]	К	[107,175]	
FeNi[Fe(CN) <sub>6</sub> ]	AI	[71]	
FeMn[Fe(CN) <sub>6</sub> ]	Na	[153,196–198]	
MnNi[Fe(CN) <sub>6</sub> ]	Na	[84,96,140,153,171]	
CoCu[Fe(CN) <sub>6</sub> ]	Na	[199,200]	
TiFe[Fe(CN) <sub>6</sub> ]	Li	[176]	
TiFe[Fe(CN) <sub>6</sub> ]	Na	[176]	
MnCoNi[Fe(CN) <sub>6</sub> ]	Na	[201]	
CuZn[Fe(CN) <sub>6</sub> ]	Zn	[178]	
TiMn[Fe(CN) <sub>6</sub> ]	Na	[202]	

 Table 1.1
 Mixed metal hexacyanoferrates as tested as battery cathodes

## **1.5 Objectives of this work**

Prussian blue analogues are an interesting family of materials whose electrochemical and physical properties make them intriguing candidates for nextgeneration electrode materials. In particular, their large interstitial spacing can accommodate a variety of ions including multivalent species, which can lead to batteries with higher energy densities than batteries based on monovalent cations. Furthermore, the ability to tune the properties of a PBA by varying the transition metals in the lattice opens the door to modifying a material to meet the particular needs of a specific application. The experimental studies in this dissertation build upon earlier work on PBAs and mixed metal hexacyanoferrates, reviewed above, and combine previously studied materials in new systems as a way to improve the electrochemical properties of Prussian blue analogue batteries. The objectives of these studies were to:

- Develop non-lithium ion based systems utilizing PBA cathodes, with a particular focus on divalent ion systems. Divalent ion batteries are of great interest as they possess double the theoretical energy density of Li<sup>+</sup> batteries for equal amounts of intercalated ions.
- 2. Determine if the physical and electrochemical storage properties of a PBA could be improved if two binary metal hexacyanoferrates are incorporated into a hybrid metal hexacyanoferrate composite. Of particular interest were what effects Co or Ni would have on stabilizing manganese in the PBA lattice.

These objectives were achieved by performing the investigations presented in the following chapters.

Chapter 2 of this dissertation explains the physical and electrochemical properties that are examined in evaluating a candidate redox system for battery usage, and the methods used to examine these properties.

Chapter 3 presents a calcium ion system containing a Prussian blue cathode. The results demonstrate the ability of PB to successfully intercalate and deintercalate Ca<sup>2+</sup> ions while maintaining high specific capacities and experiencing minimal capacity fading over extended cycling.

Chapter 4 presents a study on the mixed metal system KMn<sub>x</sub>Co<sub>1-x</sub>[Fe(CN)<sub>6</sub>] as a cathode material for aqueous zinc ion batteries (ZIBs). In general, zinc ion batteries (ZIBs) are of interest because zinc metal can be used as an anode in aqueous chemistries, unlike many other battery chemistries including sodium ion batteries (SIBs), potassium ion batteries (KIBs) and magnesium ion batteries (MIBs). The latter are either too volatile (Na and K) or suffer from non-conductive oxide formation (Mg).

Chapter 5 examines the effects of coordinated and zeolitic water on the Mg<sup>2+</sup> storage properties of copper hexacyanoferrate in a nonaqueous solvent. The inability of copper and manganese to produce a single-phase, mixed metal hexacyanoferrate will also be discussed.

Chapter 6 explores the Na<sub>2</sub>Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>] mixed metal system and its use as a cathode material for nonaqueous potassium ion batteries. The objective of this study was to increase the storage capacity of nickel hexacyanoferrate by replacing a fraction of the Ni atoms with Mn, while avoiding the known sluggish kinetics of pure manganese hexacyanoferrate

Chapter 7 introduces preliminary density functional theory results for  $Na_2Mn_xNi_{1-x}[Fe(CN)_6]$ .

Chapter 8 will provide a discussion of all of the results and their impact on the field of energy storage to conclude this investigation.

The systems investigated in chapters 3-6 are listed in Table 1.2 on the following page.

Chapter	Cathode	Cation	Electrolyte	Contribution
3	Prussian blue KFe[Fe(CN)6	Ca <sup>2+</sup>	Acetonitrile	Use of calcium as the intercalating species.
4	Manganese-cobalt hexacyanoferrate K <sub>2</sub> Mn <sub>x</sub> Co <sub>1-x</sub> [Fe(CN) <sub>6</sub> ]	Zn <sup>2+</sup>	Water	Use of zinc as the intercalating species with this system.
5	Copper hexacyanoferrate K <sub>2</sub> Cu[Fe(CN) <sub>6</sub> ]	Mg <sup>2+</sup>	Propylene carbonate and ethylene carbonate	Investigation of the role zeolitic and coordinated water have on the magnesium ion storage properties of K <sub>2</sub> Cu[Fe(CN) <sub>6</sub> ]
6	Manganese-nickel hexacyanoferrate K <sub>2</sub> Mn <sub>x</sub> Ni <sub>1-x</sub> [Fe(CN) <sub>6</sub> ]	K+	Propylene carbonate and ethylene carbonate	Use of potassium as the intercalating species. Investigation into the relationship between the percentage Mn and the bonding properties, storage capacity, and rate capability of the resulting $K_2Mn_xNi_{1-x}[Fe(CN)_6]$

## Table 1.2 Outline of work presented in this dissertation

#### Chapter 2.

#### Methods

Redox materials that are being evaluated as candidates for batteries must be characterized in terms of their physical and electrochemical properties. Several methods are used to examine these properties.

#### 2.1 Physical Properties and their measurement

As discussed earlier in the review of Prussian blue analogues, the physical properties of PBA affect their electrochemical behavior. These properties, including crystalline structure, water content, particle size and morphology, and content of transition metals, can be determined by X-ray diffraction, thermogravimetric analysis, scanning electron microscopy, energy dispersive X-ray spectroscopy, and Fourier transform infrared spectroscopy, as are discussed in section 2.2.1 through section 2.2.5.

## 2.1.1 X-ray Diffraction

Powder x-ray diffraction (XRD) is a non-destructive analytical technique used to study the crystal structure of a material. A diffraction pattern is generated by sweeping a detector over a fixed set of 2 $\Theta$  angles and measuring the x-rays scattered by the sample. The angle at which the detector will observe a signal, and the intensity of that signal, are uniquely determined by the structure and elements of the material. A sample spectrum is shown in Figure 2.1. The relationship between the diffraction pattern of a material and its crystal structure is given by Bragg's law (equation 2.1):

$$n\lambda = 2dsin(\theta) \tag{2.1}$$

where n is an integer,  $\lambda$  is the wavelength of the incident x-rays, d is the distance between atomic layers in the sample, and  $\Theta$  is the angle of incidence. For a given  $\lambda$  and the set of interatomic spacings of a given material there is a unique set of  $\theta$ 's, making every material's diffraction pattern a sort of structural signature. However, every diffraction pattern has multiple possible crystal structures that could have generated it. Thus, in order to determine the crystal structure of a sample, additional information or a



Figure 2.1 Standard powder X-ray diffraction profile

preliminary, approximate structure is required. The majority of Prussian blue analogues form a crystal structure similar to that of Prussian blue, making structure determination possible for PBAs.

For the work presented in this dissertation, a Rigaku Ultima IV with a Cu K $\alpha$  source was used to collect all XRD profile.

#### 2.1.2 Thermogravimetric Analysis

Thermogravimetric analysis (TGA) is a quantitative analytical technique that measures the mass loss of a sample by monitoring its weight as it is heated at a constant rate. TGA measurements provide information about phenomena such as off gassing of volatile compounds, moisture content, thermal stability and decomposition kinetics. Depending on the environment in which a TGA experiment is conducted, e.g. in air, inert atmosphere or O<sub>2</sub>, different reactions can also be detected.

For the work presented in this dissertation, TGA was used to study water content before and after thermal treatment, as well as determine the thermal stability of materials.

#### 2.1.3 Scanning Electron Microscopy

A scanning electron microscopy (SEM) is a type of electron microscope that produces an image by rastering a beam of incident electrons over a sample. Backscattered electrons (BSEs) are high energy electrons that reflect off atomic nuclei in the sample. Secondary electrons (SEs) are produced when an electron from the incident beam transfers enough energy to an atom in the sample to eject an electron from the sample. Secondary electron images provide more information about the topology of a sample, while back-scattered images offer high contrast.

For the work presented in this dissertation, back-scattered images were used because they provided more information about the particle size of the materials being examined.

#### 2.1.4 Energy Dispersive X-Ray Spectroscopy

Energy dispersive x-ray spectroscopy (EDS) is a semi-quantitative analytical technique that can accompany electron microscope imaging and provide information about the elemental composition of a sample. As secondary electrons are ejected from atoms during electron scanning, a higher energy, outer shell electron can settle into the newly generated vacancy and emit a photon with energy in the x-ray region of the spectrum, equal to the energy difference between the two electronic states. The x-ray energies provide signatures of the electronic structure of the emitting element and therefore allow that element to be identified.

In the work presented in this thesis, EDS was used to examine the chemical composition of mixed metal hexacyanoferrates, and to identify what ions were participating in intercalation and deintercalation during discharging and charging of electrodes.

#### 2.1.5 Fourier Transform Infrared Spectroscopy

Infrared (IR) spectroscopy probes the molecular bonds of a sample by irradiating it with infrared light and measuring the transmitted signal. Fourier transform infrared spectroscopy (FTIR) uses a broadband infrared light source and a Michelson interferometer to collect an interferogram from which an entire IR spectrum can be reconstructed by taking the Fourier transform. In practice, the interferogram is generated by shining the IR light onto a mirror with a pathlength that changes at a known frequency. The most important IR absorption peaks for PBAs are:

- 1. The C≡N stretching frequency (major peak between 1900 2200 cm<sup>-1</sup>),
- 2. Metal carbon stretching frequency (major peak between 500 600 cm<sup>-1</sup>),
- 3. Surface water (broad peak centered near 3350 cm<sup>-1</sup>),
- 4. Zeolitic water (sharp peak near 1600 cm<sup>-1</sup>), and
- 5. Coordinated water (shoulder near 1650 cm<sup>-1</sup>).

## 2.2 Electrochemical Properties

The electrical properties of candidate redox systems are quantitatively characterized by measuring specific capacity, cell potential, cycle lifetime, coulombic efficiency and rate capability. These properties are discussed below (sec. 2.2.1 – sec. 2.2.5), followed by a presentation of the methods used to evaluate these properties (sec. 2.3.1 – sec. 2.3.3).

#### 2.2.1 Specific Capacity

In stationary battery systems the most important measure of storage capacity is gravimetric capacity, or capacity per unit mass of active material. The theoretical gravimetric capacity (mAh g<sup>-1</sup>) of a material is defined as the amount of charge that can be stored per unit mass of active material. For energy stored through redox reactions, theoretical gravimetric capacity is described by

$$Capacity = \frac{n F}{3.6 M}$$
(2.2)

where Capacity is measured in mAhg<sup>-1</sup>, n is the number of moles of electrons transferred per mole of redox material, F is the electric charge carried by one mole of electrons (Faraday's constant), and M is the molar mass (g·mol<sup>-1</sup>) of the redox material.

For other applications such as mobile electronics and cars, where battery size is a major consideration, volumetric capacity is also considered.

## 2.2.2 Cell Electrical Potential

The thermodynamic parameters of a battery's redox reactions can be used to predict the battery's theoretical maximum voltage, and thereby provide valuable means for estimating the potential usefulness of chemical redox systems as battery components.

The redox reactions of batteries are described thermodynamically by

$$\Delta G^{o}_{reaction} = \Sigma \Delta G^{o}_{f} (product) - \Sigma \Delta G^{o}_{f} (reactant)$$
(2.3)

where  $\Delta G^{o}_{reaction}$  is the change in Gibbs free energy under standard conditions (of temperature and pressure), and  $\Delta G^{o}_{f}$  is the Gibbs free energy of formation under standard conditions. If there is no transfer of heat from the battery to the external world, and no external pressure-volume work is done by the battery, then  $\Delta G^{o}_{reaction}$  equals the usable electrical work of the system. The total electrical work (W) done by a battery can be expressed as:

$$W = qV \tag{2.4}$$

where q is the total charge transferred from the anode to the cathode during discharge, and V is the average voltage difference between anode and cathode during discharge. The charge transferred during a reaction is equal to nF, where n is the number of moles of electrons transferred in the reaction, and F is the charge per mole of electrons (Faraday's constant). Thus, the change in Gibbs free energy of a redox reaction is related to the cell's average voltage by

$$\Delta G = -nF|V| \tag{2.5}$$

Rearranging, this average voltage can be expressed as:

$$|V| = \frac{|\Delta G_{cell}|}{nF}$$
(2.6)

and is called the open circuit voltage,  $V_{OCV}$ , when there is no external current flowing between the anode and cathode.

#### 2.2.3 Cycle Lifetime

The cycle lifetime of a battery electrode or an entire cell is the number of chargedischarge cycles the system is able to complete before its capacity drops below some threshold criterion. Numerous factors can influence the cycle life of a material including structural transformations during charging/discharging, over-charging or overdischarging, current density, temperature and side reactions. When pairing energy storage with grid-scale electricity production, battery lifetime is of particular importance as any lost capacity means that additional energy will need to be produced from alternative, potentially fossil-fuel burning, sources.

#### 2.2.4 Coulombic Efficiency

The coulombic efficiency of a battery is defined as the ratio of the total charge output to the total charge input as follows

Coulombic Efficiency = 
$$100 x \frac{Q_{Charging}}{Q_{Discharging}}$$
 (2.7)

Efficiencies are generally reported as the ratio of the specific capacity of a battery during charging to the specific capacity during discharging. An efficiency of less than 100% indicates that some side reaction is consuming energy that cannot be recovered by reversing the reaction. The initial charge discharge cycles of many battery systems deliver

coulombic efficiencies of less than 100% due to the formation of a solid-electrolyte interphase (SEI). It is important to maintain high coulombic efficiencies over the lifetime of a battery to minimize waste energy.

#### 2.2.5 Rate Capability

The rate capability, or rate performance, of a system is a measure of the relationship between the charge/discharge currents (rate) and its maximum capacity. For intercalation electrodes, the capacity decreases with increased current densities. The rate capability of a material is affected by electronic conduction in the electrode, ionic transport in the electrolyte, ionic diffusion in the active material and electrochemical reactions at the electrode/electrolyte interface [203]. All of the factors listed contribute to the total electronic and ionic resistance of a material. The rate performance of a system is less important when high power is not required.

#### 2.3 Measurement of Electrochemical Properties

Cyclic voltammetry and galvanostatic charge discharge measurements, used to evaluate the electrochemical properties of candidate cathode materials, were conducted in a three-electrode configuration.

## 2.3.1 Three-Electrode Measurements

The normal set-up of a battery consists of only the anode and cathode, with current and voltage measurements taken between the two electrodes. This configuration introduces problems when one wants to study either the anode or cathode independent of the entire cell.

A three-electrode set-up consists of a working electrode (WE), a counter electrode (CE), and a reference electrode (RE). The RE's role is to maintain a stable potential while allowing no current to pass between it and the WE. This allows for current to flow between the WE and CE while measuring the potential of the WE with respect to the fixed reference potential. Because there is no iR drop across the electrode (i.e. no current flowing) and the potential does not change, it is possible to decouple the change in potential occurring at the cathode from that of the entire cell. Special care must be taken to select a counter electrode such that it is never limiting the current or potential of the cell. This is normally done by selecting a stable material, either a metal or carbon electrode, whose surface area is much greater than the WE's. Figure 2.2 shows a standard three-electrode electrochemical cell.

All electrochemical measurements in this dissertation were conducted in a three-electrode configuration with a PBA working electrode, an Ag/AgCl reference electrode for aqueous electrolytes or an Ag/Ag<sup>+</sup> reference electrode for nonaqueous electrolytes, and a carbon rod counter electrode. The Ag/AgCl potential is well established and is not dependent on the particular system. The Ag/Ag<sup>+</sup> potential is stable for a given setup, however it is dependent on the Ag concentration in the electrode as well as the

electrolyte. Thus, Ag/Ag<sup>+</sup> reference electrodes were calibrated by using the Fc/Fc<sup>+</sup> reaction given that it is system independent. [204]



Figure 2.2 Three-electrode electrochemical cell [181]

## 2.3.2 Cyclic Voltammetry

Cyclic voltammetry (CV) is an electrochemical technique that measures the current response to a changing potential that is swept at a constant rate between a lower and an upper cutoff potential. CV is used to study the thermodynamics and kinetics of a redox reaction. For a reversible charge transfer reaction, any cathodic or anodic reaction appears as a positive peak and negative peak, respectively, in the current vs voltage graph. A typical cyclic voltammogram for a single reversible reaction is shown in Figure **2.3** [205].



Figure 2.3 standard cyclic voltammogram for a single redox reaction [182]

The formal potential of a reaction is the mean between the cathodic and anodic peaks:

$$E_{\frac{1}{2}} = \frac{E_{cathodic} + E_{Anodic}}{2}$$
(2.8)

The kinetics of a reaction can be studied by measuring the peak anodic and cathodic currents as the scan rate is varied. For reversible redox reactions, the relationship between peak current and scan rate is described by the Randles-Sevcik equation [206]:

$$I_{peak} = 0.4463 \times \sqrt{\frac{n^3 F^3}{RT}} \times \sqrt{D} \times C_o \times \sqrt{\nu}$$
(2.9)

where  $i_p$  is the peak current (A), n is the number of electrons transferred in the reaction, F is Faraday's constant, R is the ideal gas constant, T is temperature (K), D is the diffusion coefficient (cm<sup>2</sup> sec<sup>-1</sup>),  $C_0$  is the concentration of active sites (mol cm<sup>-3</sup>), and v is the cyclic voltammogram sweep rate.

In this dissertation, cyclic voltammetry was used to determine the reduction and oxidation potentials of the PBAs studied, as well as study the kinetics of ion diffusion into and out of the cathode.

#### 2.3.3 Galvanic Charge Discharge

In galvanostatic charge discharge measurements, a constant current is applied between the working and counter electrodes in a three-electrode cell while the potential of the working electrode is measured with respect to the reference. The current is applied until the potential between the WE and the CE exceeds a set potential. For this dissertation, the specific capacity, rate capability, coulombic efficiencies, and cycle lifetime were all determined from galvanic charge discharge test.

Specific capacity of a cathode at a constant current is determined by:

Specific Capacity = 
$$\frac{I \times t}{m}$$
 (mAh g<sup>-1</sup>) (2.10)

where I is the current applied, m is the mass of the active material, and t is the time to reach the cutoff potential. The rate capability of a material is determined by measuring the change in specific capacity as a function of charge/discharge current density.

#### Chapter 3.

# High performance Prussian blue as a cathode material for nonaqueous calcium ion batteries

#### **Presentation of Published work:**

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#### 3.1 Abstract

Potassium iron hexacyanoferrate, or Prussian blue (PB), is investigated as a cathode material for nonaqueous divalent calcium ion batteries. PB is an attractive prospect due to its high specific capacity, nontoxicity, low cost, and simple synthesis. Charge/discharge performances are examined at current densities of 23 mAg<sup>-1</sup>, 45 mAg<sup>-1</sup>, 90 mAg<sup>-1</sup>, and 125 mAg<sup>-1</sup> that produced reversible specific capacities ranging from 150 mAhg<sup>-1</sup> (at 23 mAg<sup>-1</sup> current density) to over 120 mAhg<sup>-1</sup> (at 125 mAg<sup>-1</sup> current density). These are the highest storage capacities to date for a divalent calcium ion cathode over extended period of charge/discharge cycling and are comparable in performance to monovalent intercalating ions.

#### 3.2 Introduction

Divalent ions have been of interest for rechargeable batteries for many years owing to the fact that a doubly charged ion can accept two electrons for a single ion. For intercalation type batteries, this means fewer ions would need to diffuse into a lattice for a given capacity, which could result in less severe lattice distortion and more reliable cells. The most interesting candidates for multivalent ion cells are Be<sup>2+</sup>, Mg<sup>2+</sup>, and Ca<sup>2+</sup> (and Al<sup>3+</sup> if trivalent ions are included) due to their lightweight and small ionic radii. Be<sup>2+</sup> can be excluded as a candidate for multivalent ion batteries due to its rarity and toxicity. Of the remaining ions, Ca<sup>2+</sup> has the highest potential, and is very close to that of Li<sup>+</sup> (-2.87 V vs SHE compared to -3.04 V for Li). This makes Ca-ions a very attractive guest species for intercalation type batteries. Early work on Ca<sup>2+</sup> cells, however, showed that Ca metal electrodes in nonaqueous electrolytes formed a surface passivation layer that inhibited electron transfer [207–210].

Intercalation electrodes are attractive for Ca-ion batteries, where the Ca ions are not plated during discharging, but inserted into the cathode lattice followed by reduction of lattice ions. Amatucci et al. and Hayashi et al. studied the electrochemical insertion and extraction of calcium into nanocrystalline V<sub>2</sub>O<sub>5</sub> [211] and V<sub>2</sub>O<sub>5</sub> nanocomposites [209,212] while delivering high specific capacities, 200 mAhg<sup>-1</sup>, 400 mAhg<sup>-1</sup>, and 465 mAhg<sup>-1</sup> respectively, for a maximum of ten cycles. Very recently, a reversible capacity of 100 mAhg<sup>-1</sup> was achieved using a CaCo<sub>2</sub>O<sub>4</sub> cathode in a completely nonaqueous system [64]. Prussian blue analogs (A<sub>x</sub>M[Fe(CN)<sub>6</sub>]-nH2O where A is an alkali metal or alkaline earth metal, and M is a transition metal; abbreviated PBA) have also been investigated as intercalation-based cathode materials for calcium ion batteries. Ni[Fe(CN)<sub>6</sub>] [87] was used as a cathode in an aqueous system and exhibited a capacity of 50 mAhg<sup>-1</sup>, while in mixed solvent aqueous electrolytes Co[Fe(CN)<sub>6</sub>] [65] and Ba[Fe(CN)<sub>6</sub>] [56] delivered capacities of 82 mAhg<sup>-1</sup> and 55 mAhg<sup>-1</sup> respectively. Several completely nonaqueous systems with PBA cathodes have been studied, which include Co[Fe(CN)<sub>6</sub>] [61], Ni[Fe(CN)<sub>6</sub>] [66,113], and Mn[Fe(CN)<sub>6</sub>] [213,214] cathodes with maximum reversible capacities of 20 mAhg<sup>-1</sup>, 60 mAhg<sup>-1</sup>, and 110 mAhg<sup>-1</sup> respectively. PBA cathodes have shown good capacity retention over a large number of cycles. Only the maximum values reported in literature are listed above. In this work, we report our initial results of the performance of iron hexacyanoferrate, or Prussian blue, cathodes with Ca-ions in a nonaqueous acetonitrile (AN) electrolyte.

## 3.3 Materials and methods

PB (KFe<sup>3+</sup>[Fe<sup>2+</sup>(CN)<sub>6</sub>]) was synthesized using the same procedure as we have previously reported [108]. Briefly, the PB was synthesized at 60 °C by slowly adding 0.05 M ferric nitrate in 25 mL deionized (DI) water to 0.1 M potassium ferrocyanide in 25 mL DI water, under constant stirring. The blue precipitate was stirred for 2 h, followed by cleaning via centrifugation at 7000 rpm with DI water and ethanol. The precipitate was dried in an oven at 60 °C and then annealed at 150 °C under vacuum for 24 h to reduce the water content of the material.

PB cathodes were prepared by combining annealed PB powder with polyvinylidene fluoride (PVDF) which served as a binder, and multi-walled carbon nanotubes and activated carbon as conductivity enhancers in the ratio of 80:9:9:2, respectively by weight. The electrode mixture was ground using a mortar and pestle until a fine powder was achieved and then mixed with N-methyl-2-pyrolidone (NMP) to form a paste. The paste was applied onto rectangular pieces of carbon paper and dried for two hours at 150 °C under vacuum. After cooling, the electrodes were weighed to determine the amount of active material present. The finished PB cathodes (total weight on the order of 1 mg of active material, surface area 4 cm<sup>2</sup>) were weighed on an analytical balance with precision to  $\pm$  0.1 mg, and confirmed on another analytical balance of similar precision.

All electrochemical measurements were carried out on a Princeton Applied Research 273a potentiostat. The PB cathodes were characterized using cyclic voltammetry (CV) and galvanic cycling in a three-electrode setup with a graphite rod as a counter electrode and an Ag/Ag<sup>+</sup> reference electrode in a 1 M AgNO<sub>3</sub>/dry AN electrolyte. A ferrocene redox (Fc/Fc<sup>+</sup>) reference was used in the electrolyte to calibrate the Ag/Ag<sup>+</sup> potential. The solvent used in all tests was acetonitrile which was dried prior to use by passing through a column of molecular sieves. Both the potassium (KPF<sub>6</sub> in dry AN) and calcium (Ca(ClO<sub>4</sub>)<sub>2</sub>xH2O in dry AN) electrolytes were left over 3 Å molecular sieves overnight to eliminate water. Once a cell was assembled, argon was flowed in the headspace and molecular sieves were placed in the bottom of the three-electrode cells to limit any additional water absorption. All sieves were activated prior to use by heating at 150 °C in an oven overnight.

The crystallographic structure of the annealed PB powder was characterized using powder X-ray diffraction (XRD) performed on a Rigaku Ultima IV X-ray diffractometer with Cu Kα radiation. Indexing and Rietveld refinement were conducted using the Fullprof crystallographic suite [215]. Morphology and particle size were investigated through scanning electron microscopy using a FEI Sirion XL30 scanning electron microscope (SEM). Elemental content of the PB cathodes was detected using energy dispersive x-ray spectroscopy (EDX) on an Oxford Instruments EDX detector mounted on the Sirion SEM.

#### 3.4 Results and Discussion

Song et al. have shown that removal of interstitial water by annealing under vacuum leads to superior electrochemical and battery performance, as well as possible structural distortions [47]. Heating Prussian blue to 150 °C eliminates most of the water from the material [113,216]. To confirm Prussian blue's structural stability at 150 °C, XRD measurements were performed before and after annealing (Figure 3.1). The XRD patterns show no noticeable changes, indicating the material did not undergo any detectable structural changes. The annealed Prussian Blue is confirmed to have a cubic crystal structure using powder x-ray diffraction with a lattice parameter of 10.21 Å and space group Pm3m (Figure 3.2). The XRD profile displays sharp and well-defined peaks indicating good crystallinity in the sample. The SEM images affirm the good crystallinity and show



**Figure 3.1** XRD pattern of pre and post annealed Prussian blue.



**Figure 3.2** Powder XRD pattern for annealed PB. The experimental x-ray spectrum is shown in red and the Rietveld fit with the solid black line


Figure 3.3 SEM image of as prepared PB nanocubes ranging between 20 - 200 nm

cubic particles ranging between 20 nm and 200 nm (Figure 3.3).

All electrochemical measurements of PB cathodes were performed in a three-electrode system as described in the materials and methods. Figure 3.4 shows the cyclic voltammetry (CV) for PB with  $Ca(CIO_4)_2$  in dry AN with the ferrocene reference added to the electrolyte. For our system, the measured potential offset is 68 mV for Ag/Ag<sup>+</sup>, which was then added to all measurements to plot voltages with reference to Fc/Fc<sup>+</sup>. The ferrocene redox potential is roughly 2.8 V against Ca/Ca<sup>+</sup> as reported by Lipson et al. [213].



**Figure 3.4** CV for PB with Ca(ClO<sub>4</sub>)<sub>2</sub> in dry AN with the ferrocene reference added to the electrolyte. The ferrocene redox potential is -0.068 V against Ag/Ag<sup>+</sup>. To report everything against Fc/Fc<sup>+</sup>, all potentials were adjusted by adding 68 mV to each. The ferrocene redox potential was taken to be the half-wave potential of the Fc/Fc<sup>+</sup> redox couple ( $E_{1/2}$ ).  $E_{1/2}$  was estimated from  $E_{1/2}$ = ( $E_{ap}$  +  $E_{cp}$ )/2, where  $E_{ap}$  and  $E_{cp}$  are the anodic and cathodic peak potentials, respectively

The nonaqueous potassium electrolyte (KPF<sub>6</sub>/dry AN) is used as a benchmark to verify the performance of the PB cathode. Figure 3.5a shows the CV for PB in the 1M KPF<sub>6</sub> based electrolyte. Two well defined redox pairs are observed at 0.67 V and 0.44 V, and 0.01 V and 0.18 V corresponding to both Fe ions switching oxidation states. An unidentified third anodic peak is observed in the KPF<sub>6</sub> electrolyte at 0.24 V and remains for all subsequent CV tests. A similar peak also occurs when cycling the Ca-ion electrolyte and is reported by others [213]. The origin of the peak needs further exploration.



**Figure 3.5** (a) CV of PB in 1M KPF<sub>6</sub> in acetonitrile at a scan rate of 0.5 mVs<sup>-1</sup>. Cycled between [-0.68 V, 1.17 V] with respect to Fc/Fc<sup>+</sup>. (b) CV of PB in 1M Ca(ClO<sub>4</sub>)<sub>2</sub> in dry acetonitrile at a scan rate of 0.5 mVs<sup>-1</sup>. Cycled between [-0.53 V, 1.27 V] with respect to Fc/Fc<sup>+</sup>. Reference electrode for each is Ag/Ag<sup>+</sup> in acetonitrile, corrected to Fc/Fc<sup>+</sup> using a ferrocene reference.

The electrochemical properties of PB upon intercalation and deintercalation of  $Ca^{2+}$  were examined using the same cell geometry as for potassium, but with 1M  $Ca(CIO_4)_2$  in dry AN. The cyclic voltammogram for  $Ca^{2+}$  is shown in Figure 3.5b. Unlike with K<sup>+</sup>, the redox peaks of PB with Ca-ions are broad and less distinguishable. This is likely a result of higher resistance to intercalation/deintercalation of Ca-ions. The undetermined anodic peak was present again.

To determine if the new anodic peak is due to a reaction with the PB cathode, cyclic voltammetry measurements of a symmetric carbon-carbon cell with  $Ca(ClO_4)_2$  in dry acetonitrile were conducted (Figure 3.6). Despite the absence of any PB, the peak is present. The source of the peak thus does not originate from any reaction with PB, but



**Figure 3.6** CV for carbon-carbon symmetric cell with Ca(ClO<sub>4</sub>)<sub>2</sub> in dry AN. Both the anode and the cathode were graphite rods, identical to the anodes used in the PB cells.

could possibly be attributed to formation of a surface electrolyte interphase at the anode, electrolyte decomposition, or an unknown anodic reaction.

PB cathodes were subjected to galvanostatic cycling using both K<sup>+</sup> and Ca<sup>2+</sup> in dry acetonitrile to determine gravimetric capacities and rate capability of the active cathode material. For K<sup>+</sup>, two separate voltage plateaus are observed during both charging and discharging (Figure 3.7a). Specific gravimetric capacity is determined by taking the amount of time required to reach the upper cut-off potential for charging and lower cutoff potential for discharging, mass of the active cathode material and the applied current. The PB cathode with the K<sup>+</sup> based electrolyte demonstrates a reversible specific capacity of 159 mAhg<sup>-1</sup> after 10 cycles at a current density of 31 mAg<sup>-1</sup> (Figure 3.7a) [217]. The current density is determined by taking only the mass of the active material into account. Others have reported similar capacity values for sodium ions, the other highly studied monovalent ion for PBA based cathodes [47,146,147,218,219].

Upon intercalation of Ca<sup>2+</sup>, a two-step redox process is observed. The plateaus on the galvanostatic graph are less defined and broader than those during charging/discharging with K<sup>+</sup> (Figure 3.7b). To study the rate capability and durability of PB, current densities of 23 mAg<sup>-1</sup>, 45 mAg<sup>-1</sup>, and 90 mAg<sup>-1</sup> were applied to a single PB cathode. The cell was subjected to 30 cycles at the lowest and middle current densities, and 100 cycles at the highest current density. The specific capacity at the end of the first



**Figure 3.7** (a) Charge-discharge profile of PB in 1M KPF<sub>6</sub> in acetonitrile at a current density of 31 mAg<sup>-1</sup>. [-.42 V, .917 V] with respect to Fc/Fc<sup>+</sup>. (b) Charge-discharge profile of PB in 1M Ca(ClO<sub>4</sub>)<sub>2</sub> in acetonitrile at a current density of 23 mAg<sup>-1</sup>. [-0.07 V, 1.07 V] with respect to Fc/Fc<sup>+</sup>. Reference electrode for each is Ag/Ag<sup>+</sup> in acetonitrile, corrected to Fc/Fc<sup>+</sup> using a ferrocene reference.



**Figure 3.8** Reversible specific capacity vs. the number of charge/discharge cycles with  $Ca^{2+}$  at three different current densities. Cut-off voltages were -0.07 V and 1.07 V with respect to the Fc/Fc<sup>+</sup> redox couple.

cycle at 23 mAg<sup>-1</sup> is 94 mAhg<sup>-1</sup> and increases to 118 mAhg<sup>-1</sup> after completing 30 cycles. After the low current density, the cathode displays fairly constant capacity around 95 mAhg<sup>-1</sup> at the middle current density, and slightly increases from 68 mAhg<sup>-1</sup> to 74 mAhg<sup>-1</sup> after 100 cycles at the high current density (Figure 3.8). The cut-off potentials for all three current densities were [0.07 V, 1.07 V] with respect to Fc/Fc<sup>+</sup>. A significant increase in reversible capacity is observed over the first 30 cycles, a trend that has been witnessed before [47,56]. The cathode was cycled again at 23 mAg<sup>-1</sup> after completing the 100 runs at 90 mAg<sup>-1</sup>. Initially the specific capacity is 173 mAhg<sup>-1</sup>, but quickly drops to and stabilizes at a capacity of 150 mAhg<sup>-1</sup>, over 15 cycles. In this work, the charge discharge reaction for PB with Ca<sup>2+</sup> can be expressed as:

$$KFe^{II}Fe^{III}(CN)_6 \to Fe^{III}Fe^{III}(CN)_6 + K^+ + e^-$$
 (3.1)

$$KFe^{II}Fe^{III}(CN)_6 \to Fe^{III}Fe^{III}(CN)_6 + K^+ + e^-$$
 (3.2)

Equation 3.1 represents the reaction of the first charge cycle and equation 3.2 the reaction for the subsequent discharge and charge cycles. Figure 3.9 shows the first six charge-discharge cycles for PB in the 1M  $Ca(CIO_4)_2$  in dry AN electrolyte. The first charging



**Figure 3.9** First 6 charge-discharge cycles of PB in 1M  $Ca(ClO_4)_2$  in acetonitrile at a current density of 23 mAg<sup>-1</sup>. [-0.07 V, 1.07 V] with respect to Fc/Fc<sup>+</sup>. Reference electrode for each is Ag/Ag<sup>+</sup> in acetonitrile, corrected to Fc/Fc<sup>+</sup> using a ferrocene reference.

cycle has a higher capacity than all subsequent cycles, which can be accounted for K<sup>+</sup> leaving the lattice and all following cycles being due to cycling of Ca<sup>2+</sup>.

EDX spectra of an as synthesized PB electrode, fully charged electrode, and fully discharge electrode were recorded to confirm that the predominant ion intercalating into and out of the PB cathode was Ca (Figure 3.10). The large potassium peak for the as synthesized sample is expected, as potassium is present during synthesis. After cycling,



**Figure 3.10** EDX spectra of an as synthesized PB electrode, fully charged electrode, and fully discharge. All spectra normalized to the Fe peak intensity for the PB after different stages of charge-discharge cycling.

when the cathode is fully discharged, a calcium peak emerges while the potassium peak that was present initially is almost entirely gone. This indicates that after the first charge, calcium replaces potassium as the intercalating ion. During charging, the calcium peak decreases, demonstrating that calcium is reversibly intercalate into and out of PB. There is an increase in Cl and O in the discharge sample, which could be due to ClO4 entering the lattice.

Further galvanostatic charge/discharge tests were conducted on a new PB cathode in an identical setup as above, except the upper cut-off potential was increased from 1.07 V to 1.37 V with respect to Fc/Fc<sup>+</sup>. The specific capacity over 80 charge/discharge cycles at a current density of 125 mAg<sup>-1</sup> is shown in Figure 3.11. Initially the reversible capacity is 120 mAhg<sup>-1</sup> and then drops to 103 mAhg<sup>-1</sup> after 80 cycles. After 40 cycles, the cycling was paused to check the CV profile, and then galvanic cycling was resumed. This accounts for the bump in the profile after 40 cycles. The specific capacities for both PB with Ca<sup>2+</sup> tests are above the 100 mAhg<sup>-1</sup> theoretical capacity for a single step redox process, but below the theoretical capacity of 200 mAhg<sup>-1</sup> for a two-step redox reaction. This implies some of the second Fe ions are also switching redox states.

The relatively high reversible capacity of Ca-ion insertion and extraction from a Prussian Blue cathode is somewhat unexpected, given the difficulties that have been experienced with other materials over many years of research. One of the main advantages of PB over other insertion-based cathodes is the size of the lattice opening

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**Figure 3.11** Reversible specific capacity vs. the number of charge/discharge with  $Ca^{2+}$  at 125 mAg<sup>-1</sup>. Upper cut-off potential of 1.37 V vs. Fc/Fc<sup>+</sup>.

into which ions intercalate during discharge. For PB cathodes the aperture in the lattice is approximately 0.25 nm based on the radius of the cyanide ion connecting the Fe<sup>2+</sup> and Fe<sup>3+</sup> ions in the Prussian Blue lattice (the distance between iron atoms in the lattice is 0.51 nm based on powder diffraction data). This is larger than most intercalation lattices, and may allow better transport. Since Ca-ions are fairly small (ionic radius 0.114 nm) with a double charge, there will be strong electrostatic interactions between the Ca-ions, and the lattice, particularly the nitrogen atom in CN with its unbonded electron pair. Intercalation of Ca<sup>2+</sup> into PB is energetically favorable, and occurs with minimal distortion of the lattice (<2% of the lattice dimension [220]). As shown in Figure 3.5a, the sites can be clearly distinguished by cyclic voltammetry with K-ions, while redox voltages for different sites with Ca-ions are not nearly as easy to distinguish. We interpret this as being due to higher resistance to movement through the lattice for the highly charged Ca-ions.

## **3.5 Conclusion**

We have shown that iron hexacyanoferrate or Prussian blue cathodes can serve as stable host lattices for reversible intercalation of Ca<sup>2+</sup> for a potential multivalent, rechargeable battery using a nonaqueous electrolyte. A reversible capacity of 150 mAh<sup>-1</sup>, 75% of the theoretical capacity for a two-step redox reaction, was achieved for a current density of 23 mAg<sup>-1</sup> and an upper cut-off potential of 1.07 V with respect to Fc/Fc<sup>+</sup>. By increasing the upper cut-off potential to 1.37 V, a reversible capacity of 120 mAhg<sup>-1</sup> was achieved at a current density of 125 mAg<sup>-1</sup>. To date, these are the highest capacities reported over an extended number of charge discharge cycles for an intercalation-based Ca-ion battery. This work is still in progress and we expect that further optimization of the cell may lead to improved performance.

#### **3.6 Additional Commentary on Published Work**

**Kuperman N**, Padigi P, Goncher G, Evans D, Thiebes J, Solanki R. High performance Prussian Blue cathode for nonaqueous Ca-ion intercalation battery. Journal of Power Sources 2017;342:414–8. <u>https://doi.org/10.1016/j.jpowsour.2016.12.074</u>. [117]

The results obtained in this study helped to accomplish the goal of developing non-lithium ion based systems utilizing a PBA cathode by demonstrating, for the first time, the suitability of Ca<sup>+2</sup> as an electrolytic cation in the battery system consisting of a Fe[Fe(CN)<sub>6</sub>] cathode and acetonitrile solvent. In fact, with a specific capacity of 150 mAhg<sup>-1</sup>, the PB cathode described in this work delivered the highest reported specific capacity for any calcium ion battery utilizing a PBA electrode. Divalent calcium ion batteries are of particular interest due to calcium's low cost, relative abundance (fifth most abundant element in the Earth's crust), and ability to offer double the energy density, per intercalated ion, compared to lithium ion batteries. By employing a nonaqueous chemistry, this work offers a proof of concept to future studies aimed at developing a CIB with a calcium metal anode.

#### Chapter 4.

# Manganese-Cobalt Hexacyanoferrate as a Cathode Material for Aqueous Zinc ion Batteries

#### **Presentation of Published Work**

**Kuperman N**, Hopkins M, Olson S, Goncher G, Evans D, Solanki R. Cathode Material Composed of Manganese Cobalt Hexacyanoferrate Nanoparticles for Aqueous Zinc Ion Intercalation Batteries. 2018 IEEE 13th Nanotechnology Materials and Devices Conference (NMDC), 2018, p. 1–4. <u>https://doi.org/10.1109/NMDC.2018.8605900</u>. [221]

#### 4.1 Abstract

To accommodate the global shift towards increased energy production from renewable sources, further advancements in storage technology are needed to mitigate the intermittent nature of wind and solar. Aqueous zinc ion intercalation batteries (ZIBs) offer an inexpensive and safe alternative to the traditional lithium ion battery (LIB), making them a prime candidate for large scale storage. Metal hexacyanoferrates have been shown to be suitable cathode materials for ZIBs, allowing for the reversible insertion/extraction of the doubly charged zinc ion. In this work, we report on the performance of a cathode material composed of mixed manganese-cobalt hexacyanoferrate nanoparticles for a rechargeable ZIB. The cathode exhibits a reversible capacity of 111 mAhg<sup>-1</sup> at 25 mAg<sup>-1</sup> and good capacity retention after extended cycling at 100 mAg<sup>-1</sup>. X-ray diffraction and SEM imaging reveal nanoparticles with a rhombohedral structure and sizes on the order of 20 – 60 nm. The combination of the nontoxic hexacyanoferrate cathode, with the aqueous zinc ion electrolyte offers a promising system for large scale energy storage.

### 4.2 Introduction

In recent years, greenhouse gas emissions and global warming have become issues at the forefront of the global awareness. In 2015, the U.S. alone generated 567 terawatt hours of electricity from renewable energy sources, a 16.7% growth from the previous year [222]. This shift was mirrored worldwide as 19.3% of the global final energy consumption was provided by renewable energy [223]. However, the two main sources of renewables, solar and wind, are limited by their intermittent nature. To make these technologies viable on a large scale, novel energy storage technology is needed.

Lithium ion batteries (LIBs) have been an industry standard for energy storage due to their high gravimetric capacity, energy density, Coulombic efficiency, and long cycle lifetime. Despite their successes, the rising cost of lithium metal, as well as the toxicity and flammability of the batteries, reduce their applicability in grid scale energy storage. Aqueous zinc-ion batteries (ZIBs) are safe and nontoxic, while zinc metal and zinc salts are abundant and inexpensive, making ZIBs a potential alternative to LIBs. However, only a limited number of materials have been shown to reversibly intercalate zinc ions, including: MnO [224,225], MnS [226],  $V_2O_5$  [227,228], and Prussian blue analogues [119,229].

Prussian blue (PB) and its analogues (PBAs) are mixed valence compounds with open framework structures that can accommodate a wide variety of intercalating species in the interstitial spacing [230,231]. They possess the general formula  $A_xM_1[M_2(CN)_6]_y$ •1-y•H<sub>2</sub>O (where A is an alkali cation; M<sub>1</sub> is the n-coordinated transition metal; [M<sub>2</sub>(CN)<sub>6</sub>] is the hexacyanometallate anion; and is a M<sub>2</sub>(CN)<sub>6</sub> vacancy; 0 < x < 2; 0 < y < 1). Both transition metals can be electrochemically active in this structure, giving PBAs a high theoretical capacity (171 mAhg<sup>-1</sup> for Prussian blue, Fe[Fe(CN)<sub>6</sub>]).

In this work, we investigate hybrid manganese-cobalt hexacyanoferrate nanoparticles and their application to aqueous zinc ion batteries. The material displays reversible zinc intercalation and delivers specific capacities of 111 mAhg<sup>-1</sup> at 25 mAg<sup>-1</sup> and 75 mAhg<sup>-1</sup> at 100 mAg<sup>-1</sup>. The incorporation of manganese into the cobalt hexacyanoferrate lattice is shown to lead to improved energy storage properties.

# 4.3 Experimental

Manganese hexacyanoferrate was synthesized using the coprecipitation method described in our previous publications with slight adjustments [65,231]. An 80 mL aqueous solution of  $MnCl_2$  (40 mM), and an 80 mL aqueous solution of  $K_4Fe(CN)_6$  (20 mM)

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were slowly added simultaneously and dropwise into 40 mL NaCl (5M aq) under constant stirring and at 60 °C. The solution was stirred for two hours and the resulting precipitate was collected and washed via centrifugation with DI water and ethanol, and dried in air overnight. Once dry, the precipitate was loaded into a tube furnace and annealed under vacuum overnight at 150 °C. The Annealing process has been shown to reduce interstitial water, and lead to superior electrochemical and battery performance [47].

The same procedure was followed to synthesize cobalt hexacyanoferrate and manganese-cobalt hexacyanoferrate except that 40(1-x) mM MnCl<sub>2</sub> and 40x mM CoCl<sub>2</sub> (where x = 0.50, 1.0) were dissolved in a common 80mL aqueous solution. The resulting materials are denoted as MnHCF, MnCoHCF0.50, and CoHCF for manganese hexacyanoferrate, manganese-cobalt hexacyanoferrate, and cobalt hexacyanoferrate, respectively.

The crystal structures of the synthesized materials were characterized using powder X-ray diffraction (XRD) performed on a Rigaku Ultima IV X-ray diffractometer with Cu K $\alpha$  radiation ( $\lambda$  = 1.54056 Å). Indexing and refinement of the structures were conducted using the Fullprof crystallographic suite [215]. Morphology and chemical composition of the nanoparticles were examined by a scanning electron microscope (SEM) and energy dispersive x-ray spectroscopy (EDS) using a Zeiss Sigma VP.

Battery cathodes were prepared by combining an annealed powder with polyvinylidene fluoride (PVDF) that served as a binder, and multi-walled carbon

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nanotubes and activated carbon as conductivity enhancers in the ratio of 80:9:9:2, respectively by weight. The combined mixture was ground using a mortar and pestle until a fine power was achieved, after which N-methyl-2-pyrolidone (NMP) was added drop by drop until a paste with paint-like consistency was formed. The electrode paste was applied to both sides of a carbon paper current collector, dried for two hours at 150 °C under vacuum, and let to cool slowly overnight while still under vacuum.

The redox potentials and electrochemical properties of the metal hexacyanoferrate cathodes were characterized using cyclic voltammetry (CV) and galvanic cycling (GC) in a three-electrode setup. Cells were assembled with a graphite rod counter electrode, Ag/AgCl (in 3M NaCl) reference electrode, metal hexacyanoferrate working electrode, and 1M Zn(ClO<sub>4</sub>)<sub>2</sub> aqueous electrolyte.

## 4.4 Results and Discussions

#### 4.4.1 Structural Characterization

The XRD pattern for each material reveals structures that differ from the wellknown face-centered cubic lattice of Prussian blue (Figure 4.1a). CoHCF and MnCoHCF0.50 both index to rhombohedral lattices with space group in good agreement with other CoHCF samples synthesized in an ion rich environment [150,153]. The incorporation of Mn into the CoHCF framework results in a decreasing refraction angle for the <202> and <404> peaks (Figure 4.1b). This corresponds to an increasing lattice parameter, attributed to the substitution of the smaller octahedrally coordinated, high



**Figure 4.1** (a) XRD pattern of CoHCF, MnCoHCF0.50 and MnHCF (b) Highlighted shift in the 202 and 404 peaks for MnCoHCF0.50

spin Co<sup>2+</sup> (88.5 pm) with the large octahedrally coordinated, high spin Mn<sup>2+</sup> (97 pm) [150,232]. Additionally, the indexing to a single rhombohedral phase for MnCoHCF0.50 indicates incorporation of both Mn and Co into the lattice instead of the formation of CoHCF and MnHCF individually. MnHCF crystallized in a monoclinic geometry, differing from the commonly reported hexagonal or cubic phases [150,233]. A monoclinic structure has been observed for MnHCF synthesized at an elevated temperature [234]. Cell parameters for each material, along with their respective space group, are provided in Table 4.1.

Material	Structure	Space Group	а	b	C	α	β	γ
CoHCF	Hexagonal	R3m	10.502	10.502	10.114	90	90	90
MnCoHCF0.50	Hexagonal	R∃m	10.546	10.546	10.546	90	90	90
MnHCF	Monoclinic	<u>P2</u> m	18.896	5.528	18.156	90	94.42	90

**Table 4.1** Lattice parameters and space group assignment for each sample



Figure 4.2 SEM images of (a) CoHCF (b) MnCoHCF0.50 (c) MnHCF



Figure 4.3 EDS spectra for MnCoHCF0.50

SEM imaging for the CoHCF and MnCoHCF0.50 revealed nanoparticles on the order of 20 – 60 nm, aggregated in larger agglomerations, while MnHCF formed nanocubes on the order of 20 - 100 nm (Figure 4.2a - c). The small size of the nanoparticles offers shorter diffusion pathways for Zn ions to intercalate into the bulk of the material. The EDS spectra MnCoHCF0.50 verifies the presence of Mn in the sample (Figure 4.3).

#### 4.4.2 Electrochemical Characterization

The electrochemical redox properties of the three metal hexacyanoferrates were examined by cyclic voltammetry (scan rate of 0.5 mV/s) that revealed reversible Zn intercalation within the water voltage window for CoHCF and MnCoHCF0.50 (Figure 4.4). In Figure 4.4a, one major oxidation peak at 0.81 V, and two shoulder peaks at 0.76 V and 0.88 V, and three distinct reduction peaks at 0.59 V, 0.67 V, and 0.78 V for CoHCF, demonstrate the presence of multiple insertion/extraction reactions. Complex redox reactions, including the  $Co^{2+}/Co^{3+}$  switch, have been reported with a range of intercalating ions [87,235]. This is in contrast to CoHCF and Na<sup>+</sup> where a single broad redox peak, attributed to the Fe<sup>2+</sup>/Fe<sup>3+</sup> switch, is observed [236]. MnCoHCF0.50 exhibited three, well defined, oxidation peaks at 0.75 V, 0.81 V, and 0.90 V, and corresponding reduction peaks at 0.59 V, 0.66 V, and 0.76 V with peak currents slightly larger than its CoHCF counterpart. Unlike the other two materials, MnHCF displayed irreversible electrochemical behavior in the aqueous Zn environment. The unstable nature of MnHCF in aqueous electrolytes has been previously reported [179,192].



Figure 4.4. CV profile at 25 mV/s (a) COHCF (b) MnCoHCF0.50

Galvanic cycling (GC) was performed on MnCoHCF0.50 to further investigate the material's energy storage properties. The charge and discharge capacities of CoHCF were

taken as baselines to better understand the impact of incorporating Mn into the hexacyanoferrate lattice. Figure 4.5a shows the GC potential profiles of CoHCF and MnCoHCF0.50 at a current density of 25 mAg<sup>-1</sup> cycled between 0.0 and 1.0 V vs Ag/AgCl. The plateau between 0.64 V and 0.9 V is an indication of bulk intercalation of Zn ions and corresponds well with the redox potentials revealed in the CV measurements. The galvanic profiles for CoHCF and MnCoHCF0.50 after the first cycle (111 mAhg<sup>-1</sup>) exceeds that of CoHCF (82 mAhg<sup>-1</sup>), demonstrating the positive effect of Mn incorporation. The semiquantitative chemical compositional data gathered from EDS measurements suggest Co exists in a much greater quantity than Mn in MnCoHCF0.50; However, small levels of a third metal atom incorporated into the Prussian blue lattice have shown to improve the structural, electrochemical, and energy storage properties of the material [172].

Extended cycling at various current densities demonstrates the improved rate capability and high capacity retention of MnCoHCF0.50 compared to CoHCF. Figure 4.5 shows the specific capacity and coulombic efficiency at 25 mAg<sup>-1</sup>, 100 mAg<sup>-1</sup>, and 25 mAg<sup>-1</sup> again, over an extended number of cycles. The MnCoHCF0.50 cathode delivers a discharge capacity of 111 mAhg<sup>-1</sup> with a coulombic efficiency of 92%, whereas CoHCF delivers 82 mAhg<sup>-1</sup> with an efficiency of 92%. After 15 cycles, both MnCoHCF0.50 and CoHCF see a decay in capacity (91 mAhg<sup>-1</sup> and 75 mAhg<sup>-1</sup> respectively) while both of the coulombic efficiencies approach 100%. After 100 cycles at 100 mAg<sup>-1</sup> MnCoHCF0.50 exhibits good rate capability and retention, delivering a specific capacity of 75 mAhg<sup>-1</sup>,



**Figure 4.5** (a) 1st Galvanic Charge Discharge cycles for CoHCF and MnCoHCF0.50 (25 mA/g) (b) Specific capacity vs cycle life

while retaining 93% of its initial capacity over 100 cycles. CoHCF shows similar capacity retention, however the delivered specific capacity is lower (62 mAhg<sup>-1</sup>). Further confirming the stability of each material, MnCoHCF recovered 75% of its initial capacity after returning to 25 mAg<sup>-1</sup>, while CoHCF delivered 93% of the starting capacity.

# 4.4.3 Conclusion

In this work, MnCoHCF0.50 was successfully synthesized. XRD analysis of MnCoHCF0.50 coupled with EDS measurements confirmed a single phase with uniform distribution of Mn and Co throughout. A complex insertion/extraction process was highlighted by three distinct oxidation and reduction potentials. An increase in specific capacity was achieved by the addition of Mn to the CoHCF lattice, resulting in a 29 mAhg<sup>-1</sup> increase when cycled at 25 mAg<sup>-1</sup>. The capacity retention at an elevated current density of MnCoHCF0.50 (93% retention over 100 cycles at 100 mAg<sup>-1</sup>) indicated that the material could be a promising candidate for aqueous zinc ion batteries.

## 4.5 Additional Commentary on Published Work

**Kuperman N**, Hopkins M, Olson S, Goncher G, Evans D, Solanki R. Cathode Material Composed of Manganese Cobalt Hexacyanoferrate Nanoparticles for Aqueous Zinc Ion Intercalation Batteries. 2018 IEEE 13th Nanotechnology Materials and Devices Conference (NMDC), 2018, p. 1–4. <u>https://doi.org/10.1109/NMDC.2018.8605900</u>. [221]

The studies presented in this chapter were undertaken to:

- 1. Develop non-lithium ion based systems utilizing PBA cathodes, with a particular focus on divalent ion systems.
- Determine if the electrochemical storage properties of pure cobalt hexacyanoferrate and pure manganese hexacyanoferrates could be improved by incorporating both Co and Mn into the same lattice.

The results obtained in this study helped to accomplish these goals by demonstrating:

- For the first time, the successful use of Zn<sup>+2</sup> with Co[Fe(CN)<sub>6</sub>] and MnCo[Fe(CN)<sub>6</sub>] cathodes in an aqueous solvent, and
- Synergistic properties of Mn and Co in the mixed metal hexacyanoferrate MnCo[Fe(CN)<sub>6</sub>].

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The incorporation of Mn into a CoHCF lattice, producing MnCoHCF0.50, resulted in a 21% increase in reversible specific capacity in the aqueous electrolyte. Furthermore, Co stabilized the Mn-N=C-Fe chain and prevented dissolution into an aqueous electrolyte. However, a negative effect on electrochemical properties was observed, which was an increased capacity loss for MnCoHCF0.50 compared to CoHCF, 18% vs. 9% respectively, after the first 15 charge-discharge cycles. Two reasons zinc ion batteries of interest are their high theoretical energy densities due to Zn being divalent, and the ability to use zinc metal with aqueous chemistries. Aqueous systems have high safety profiles and low environmental impact, compared to nonaqueous systems.

#### Chapter 5.

Copper Hexacyanoferrate as a cathode material for magnesium ion batteries.

## 5.1 Prelude

The original goal of this study was to investigate manganese-copper hexacyanoferrate (MnCuHCF) as a cathode material for magnesium ion batteries. However, XRD revealed Mn and Cu formed a multi-phase product when synthesized by coprecipitation in 5M NaCl at 60  $^{\circ}$ C (Figure 5.1).



**Figure 5.1** XRD profiles for the hydrated samples of copper hexacyanoferrate (CuHCF), manganese-copper hexacyanoferrate (MnCuHF0.50), and manganese hexacyanoferrate (MnHCF)

After completing the study on copper hexacyanoferrate cathode for magnesium ion batteries, two novel hydrothermal synthesis methods were developed that produced single phased Na<sub>2</sub>Mn<sub>0.50</sub>Cu<sub>0.50</sub>[Fe(CN)<sub>6</sub>], denoted as MnCuHCF0.50. In a typical synthesis 20 mM of CuCl<sub>2</sub>·2H<sub>2</sub>O and 20 mM of MnCl<sub>2</sub>·2H<sub>2</sub>O were dissolved in 35 mL of deionized (DI) water, and 20 mM of K<sub>4</sub>Fe(CN)<sub>6</sub> was dissolved separately in 35 mL of DI water. The two solutions were transferred to a 100 mL Teflon lined stainless steel autoclave with either 20 mL sodium citrate (0.2 M aq) or sodium sulfate (1.5 M aq), sealed, and maintained at 120 °C for 12 hours. The resulting was collected and washed via centrifugation with DI water followed by a final wash with ethanol.

The XRD profiles for the citrate and sulfate syntheses, denoted as C-MnCuHCF0.50 and S-MnCuHCF0.50 respectively, are shown in Figure 5.2. SEM imaging and the



**Figure 5.2** XRD profiles for hydrothermal synthesis of MnCuHCF0.50 with sodium citrate (blue) and sodium sulfate (orange). Both samples crystalized into a single phase.



**Figure 5.3** (a) SEM image of C-MnCuHCF0.50 (b) EDS elemental map of C-MnCuHCF0.50.

accompanying EDS elemental map reveal an even distribution of both Mn and Cu throughout C-MnCuHCF0.50 (Figure 5.3 a,b). The higher stability constant for the copper citrate complex compared to the manganese citrate explains the higher concentration of Mn compared to Cu [237].

The relationship between the synthesis conditions and a mixed metal hexacyanoferrates formation offers an intriguing avenue to explore in future work.

#### **Presentation of Published Work**

**Kuperman N**, Cairns A, Goncher G, Solanki R. Structural water enhanced intercalation of magnesium ions in copper hexacyanoferrate nonaqueous batteries. Electrochimica Acta 2020;362:137077. <u>https://doi.org/10.1016/j.electacta.2020.137077</u>. [238]

## 5.2 Abstract

In this article we investigate copper hexacyanoferrate (CuHCF) as a nonaqueous magnesium ion battery (MIB) cathode, and the positive influence of structural water on its Mg<sup>2+</sup> storage properties. The hydrated and dehydrated forms of CuHCF (H- and D-CuHCF) each displayed excellent rate capabilities and extended lifetimes with zero capacity loss. However, H-CuHCF delivers a specific capacity 25% higher than that of D-CuHCF. Cyclic voltammetry and galvanostatic charge discharge reveal a redox reaction present only in the hydrated CuHCF, which accounts for 25% of its total reversible capacity (63 mAh g<sup>-1</sup> at 25 mA g<sup>-1</sup>). Furthermore, ex-situ FTIR reveals that the structural water of H-CuHCF remains in the lattice during charging/discharging. We propose that water provides partial electrostatic screening between the CuHCF lattice and Mg ions, while allowing an additional redox transition to become thermodynamically accessible.

#### 5.3 Introduction

As the overall cost of energy production from renewable sources continues to drop globally [239], a lack of robust energy storage solutions is curtailing wide scale adoption of renewables and decarbonization of the energy economy [240,241]. Rechargeable batteries are one possible solution to the demand for storage, with the lithium ion battery (LIB) being the current standard. However, due to the cost, safety concerns, and toxicity of LIBs, new battery technologies are needed to fully utilize renewable energy sources, such as wind and solar.

One promising alternative to LIBs is the divalent magnesium ion battery (MIB), as magnesium is relatively abundant, stable in air, and environmentally benign. Additionally, magnesium metal anodes possess high volumetric and gravimetric capacities (3833 mAh cm<sup>-3</sup> and 2205 mAh g<sup>-1</sup> for Mg vs. 2046 mAh cm<sup>-3</sup> and 3861 mAh g<sup>-1</sup> for Li) and can be plated safely without dendritic growth [242–244]. Unfortunately, sluggish kinetics and high migration barriers have made the development of suitable MIB cathodes challenging [57]. Some advances have been made on MIB cathodes that are able to reversibly intercalate Mg<sup>2+</sup>, including: Mg<sub>x</sub>Mo<sub>3</sub>S<sub>4</sub> [243], Mg<sub>x</sub>Cu<sub>y</sub>Mo<sub>6</sub>S<sub>8</sub> [58], MnO<sub>2</sub>[245], V<sub>2</sub>O<sub>5</sub> [246], and Prussian Blue analogues (PBAs) [111,113].

Prussian Blue analogues are a family of mixed valence compounds with a general composition of  $A_xM_1[M_2(CN)_6]_y \bullet \Box_{1-y} \bullet zH_2O$  (where A is an alkali cation;  $M_1$  is the N-coordinated transition metal;  $M_2(CN)_6$  is the hexacyanometallate anion; and  $\Box$  is a

 $[M_2(CN)_6]^{3-/4-}$  vacancy; 0 < x < 2; 0 < y < 1). Water molecules can be present in two unique crystallographic environments: coordinate to the unbonded  $M_1$  atoms replacing the missing hexacyanometallate anions (coordinated water), and additional water can reside in the interstitial spacing (zeolitic water).

From neutron diffraction studies, the distinct water sites for a generic cubic PBA have been identified as: zeolitic water residing at the 8c position in the center of the lattice (A-site), and coordinated water at the 24e position (B-site) close to the location of the missing nitrogen as shown in Figure 5.4 [125].

There has been extensive research on PBAs for energy storage applications for both aqueous and nonaqueous systems owing to their large open framework, structural stability, high theoretical capacity (170 mAh g<sup>-1</sup>), and ability to accommodate a wide variety of intercalating species [65,85,87,113,115,123,150,201,221,230,231,244].

Coordinated and zeolitic water play an integral role in the electrochemical properties of a PBA, having positive and negative effects depending on the system of interest. For aqueous electrolytes, water offers charge screening between the lattice and the intercalating ions, which allows for high ionic mobilities on the order of 10<sup>-7</sup> cm<sup>2</sup> s<sup>-1</sup> [150]. Additionally, zeolitic and nitrogen coordinated water can facilitate the migration of ions in PBAs [87]. For some nonaqueous systems, the removal of water from the PBA lattice during cycling results in parasitic side reactions and structural degradation [80]. Efforts to mitigate these negative effects of water has led to considerable research on the



**Figure 5.4** Depiction of the cubic structure of CuCHF (a) A pristine lattice where intercalated ions can reside at A lattice sites (8c). (b) B lattice site (24e) of CuHCF at a  $[M_2(CN)_6]^{3-/4-}$  vacancy and the resulting coordinated water molecules bonded to the dangling Cu<sup>2+</sup> atoms.

development of low vacancy materials with minimal water content [55,201]. However, Padigi et al. and others have demonstrated the successful use of hybrid aqueous/nonaqueous electrolytes can improve electrochemical performances and increase specific capacities by more than 45% [65,151].

In this work, we have investigated the impact of coordinated and zeolitic water on the electrochemical and energy storage properties of copper hexacyanoferrate (CuHCF), and its use as a cathode material for nonaqueous MIBs. The dehydrated copper hexacyanoferrate displays inferior electrochemical energy storage properties compared to the hydrated form, counter to many other PBAs whose performance improves upon the removal of water as part of the synthesis procedure [47,55]. Through a combination of FTIR, ex-situ energy dispersive x-ray spectroscopy (EDS), cyclic voltammetry (CV), and galvanic charge discharge we confirm the reversible intercalation of Mg<sup>2+</sup> ions and examine the effect of zeolitic and coordinated water on Mg intercalation.

## 5.4 Materials and Methods

## 5.4.1 Materials Synthesis:

CuHCF was synthesized by coprecipitation similar to our previous work, with slight modification [221]. Briefly, 40 mM of CuCl<sub>2</sub>·2H<sub>2</sub>O was dissolved in 80 mL of deionized (DI) water, and 20 mM of K<sub>4</sub>Fe(CN)<sub>6</sub> was dissolved separately in 80 mL of DI water. The two solutions were simultaneously added dropwise into 40mL NaCl (5M aq) under constant stirring and maintained at 60 °C for two hours. The resulting precipitate was collected and washed via centrifugation with DI water followed by a final wash with ethanol. Materials were dried under two conditions: (1) dried in air overnight, denoted as the hydrated copper hexacyanoferrate (H-CuHCF) and (2) dried in air overnight and annealed at 100 °C under vacuum for two hours, denoted as the dehydrated copper hexacyanoferrate (D-CuHCF). The water content of these two materials differ substantially, which has a large effect on their energy storage properties.
#### 5.4.2 Material Characterization:

The crystal structure of each sample was characterized using powder x-ray diffraction (XRD) performed on a Rigaku Ultima IV X-ray diffractometer with Cu K $\alpha$  radiation ( $\lambda$ =1.54056 Å). Indexing and refinement of the structures were conducted using the Fullprof crystallographic suite [215,247]. Morphology and chemical composition of the nanoparticles and fully assembled cathodes were examined by scanning electron microscope (SEM) and energy dispersive x-ray spectroscopy (EDS) using a Zeiss Sigma VP SEM. Thermal and water content analysis was performed using a thermogravimetric analyzer (TGA, Mettler TGA-50) from 50 to 300 °C at a heating rate of 5 °C min<sup>-1</sup> under flowing N<sub>2</sub>. Fourier transform infrared spectroscopy (FTIR, Thermo Scientific Nicolet iS10 FTIR equipped with diamond ATR) in the range of 600 - 3800 cm<sup>-1</sup> was used to probe the chemical environment of the cyanide ligand and determine the oxidation states of the transition metals. FTIR in the range of 90 – 690 cm<sup>-1</sup> was performed on a Thermo Scientific Nicolettie 6700 equipped with a DTGS detector to probe the metal-carbon and metal-nitrogen bonding.

## 5.4.3 Electrochemical Measurements:

All electrochemical measurements were performed using a Gamry reference-600 potentiostat in a 3-electrode setup. Cathodes were prepared by coating a slurry of either H-CuHCF or D-CuHCF, polyvinylidene fluoride (PVDF), multi-walled carbon nanotubes, and activated carbon in the ratio of 80:9:9:2, respectively by weight in N-methyl-2-pyrolidone (NMP) onto carbon paper. The coated electrodes were cured for two hours at 100 °C

90

under vacuum prior to use. In general, cells consisted of the respective cathode, a carbon rod counter, an Ag/Ag<sup>+</sup> in propylene carbonate reference, and an electrolyte of 1 M magnesium perchlorate anhydrous, Mg(ClO<sub>4</sub>)<sub>2</sub>, in a mixture of propylene carbonate (PC) and ethylene carbonate (EC) [PC/EC = 50/50 by volume]. All reference electrodes were calibrated against the Fc/Fc<sup>+</sup> redox couple. Additionally, all electrolytes were dried over 3 Å molecular sieves to remove any residual water.

## 5.5 Results and Discussion

Powder x-ray diffraction was used to characterize changes in the crystal structure of CuHCF after thermal treatments. The powder XRD patterns for hydrated and dehydrated CuHCF are shown in Figure 5.5a. H-CuHCF exhibits sharp peaks indicative of high crystallinity and can be indexed to the well-known face-centered cubic structure with a lattice parameter of 10.03 Å. After annealing at 100 °C for two hours, D-CuHCF undergoes a phase change to an orthorhombic system with lattice parameters a = 10.32 Å, b = 10.21 Å, c = 9.88 Å. Profile fits to the cubic and orthorhombic crystal structures are shown in Figure 5.6. PBAs are known to undergo structural distortions during thermal treatments, caused by the removal of both zeolitic and coordinated water [47]. The orthorhombic phase of D-CuHCF is consistent with other reported Prussian blue analogue systems such as NiNa<sub>2</sub>[Fe(CN)<sub>6</sub>]·2H<sub>2</sub>O [248], Cs<sub>0.97</sub>Cu[Fe(CN)<sub>6</sub>]<sub>0.99</sub>·1.1H<sub>2</sub>O [249], and CoK<sub>2</sub>[Fe(CN)<sub>6</sub>]·2H<sub>2</sub>O [250]. Upon dehydration at 150 °C, the CuHCF cubic or slightly distorted cubic crystal structure is no longer present indicating a breakdown of the



**Figure 5.5** Physical characterization of H- and D-CuHCF. (a) Powder x-ray diffraction patterns for D-CuHCF and H-CuHCF. (b) Thermogravimetric curves for the CuHCF powders. H-CuHCF undergoes a 34% mass loss due to the removal of both zeolitic and coordinated water between 50 °C < T < 115 °C. D-CuHCF experiences an 8% mass loss over the same temperature range. (c) FTIR spectra (between 600 - 3800 cm<sup>-1</sup>) confirm the removal of surface water (3350 cm<sup>-1</sup>), and partial removal of coordinated and zeolitic water (1650 and 1610 cm<sup>-1</sup>, respectively). (d) FTIR spectra in the far IR range (between 90 – 690 cm<sup>-1</sup>) demonstrate the effect of dehydration on the Fe-CN and Cu-N bond.



**Figure 5.6** XRD profile fittings for **(a)** The cubic structure of H-CuHCF with lattice parameter 10.03 Å **(b)** The orthorhombic structure of D-CuHCF with lattice parameters a = 10.32 Å, b = 10.21 Å, c = 9.88 Å.

material (Figure 5.7). SEM imaging reveals nanosized particles on the order of 25 – 100 nm which aggregate into larger agglomerations (Figure 5.8).

Levels of hydration and forms of water in each sample were evaluated with thermogravimetric analysis and FTIR. Figure 5.5b shows the TGA curves of both samples. H-CuHCF displays a distinct mass loss step between 50 °C < T < 115 °C, which corresponds to the removal of both zeolitic and coordinated water (34 % mass loss) [85,251]. Above 115 °C the material begins to gradually decompose. This behavior is similar to previous reports of copper hexacyanoferrate [85]. D-CuHCF shows an 8% weight loss between 50 °C < T < 115 °C, indicating the successful removal of 67% of the coordinated and zeolitic water. The mass gain at 170 °C for D-CuHCF is likely due to the breakdown of the hexacyanoferrate structure, followed by a secondary exothermic reaction [251]. CuHCF is



**Figure 5.7** Powder x-ray diffraction patterns for CuHCF after different thermal treatments: annealed under vacuum at 150 °C, annealed under vacuum at 100 °C (D-CuHCF), untreated (H-CuHFC) and the crystalline structure breaks down after the high temperature anneal



**Figure 5.8** Standard SEM image of CuHCF. CuHCF crystalizes into nano-sized particles on the order of 25-100 nm, and further aggregate into large agglomerations.

known to be thermally unstable compared to other PBAs that can withstand annealing temperatures above 100 °C without any structural change or degradation [252].

The FTIR spectra in Figure 5.5c shows a large absorption peak for both H- and D-CuHCF at 2090 cm<sup>-1</sup> of the CN stretching frequency, v(C=N), which is characteristic of Cu<sup>II</sup>-NC-Fe<sup>II</sup>. A small splitting is observed in D-CuHCF, which is attributed to the structural shift to a lower crystal symmetry [253]. Neither sample exhibits v(C=N) of Cu<sup>II</sup>-NC-Fe<sup>III</sup> (located at 2174 cm<sup>-1</sup>), confirming the homogeneity of the iron oxidation state in the

as-prepared materials. For H-CuHCF, the broad absorption peak centered at 3350 cm<sup>-1</sup> is due to the O-H stretching frequency of free surface water, while the bending modes of weakly bound zeolitic water and coordinated water are associated with the sharp peak 1610 cm<sup>-1</sup> and the shoulder at 1650 cm<sup>-1</sup>, respectively [251]. Upon dehydration, the broad surface water peak is removed while the IR bands associated with both zeolitic and coordinated water are weakened, further verifying their partial removal.

The FTIR spectrum of a cured H-CuHCF electrode confirms the coordinated and zeolitic water remains in the lattice while all surface water is removed (Figure 5.9). The stability of water in the prepared electrode compared to D-CuHCF is attributed to the presence of the PVDF binder which may help trap the water within the lattice. It should be noted that curing corresponds to the heating of the entire electrode material, whereas annealing refers to exclusively heating the bare CuHCF powder.

Far IR spectra in the rage of 90 - 690 cm<sup>-1</sup>, shown in Figure 5.5d, were taken to study the relationship between coordinated and zeolitic water and the metal cyanide bonds. For H-CuHCF, the peaks at 598 cm<sup>-1</sup> and 264 cm<sup>-1</sup> are due to the Fe-CN linear bending and Cu-N asymmetric stretching modes respectively [253]. The corresponding D-CuHCF bands are redshifted by 4 cm<sup>-1</sup>, indicating that the removal of water results in a weakening of the bonds. Interestingly, the Fe-C stretching modes located 491 and 452 cm<sup>-1</sup> remain unchanged in these samples.



**Figure 5.9** FTIR spectra of H-CuHCF pre- and post-curing at 100 °C under vacuum, confirming coordinated and zeolitic water are not removed from the H-CuHCF electrodes. The stability of the coordinated and zeolitic water is attributed to the presence of the PVDF binder.

The redox properties of the samples upon intercalation of Mg<sup>2+</sup> were investigated by cyclic voltammetry in a three-electrode configuration at a sweep rate of 0.5 mV s<sup>-1</sup> (Figure 5.10). Electrochemical measurements were corrected using a ferrocene calibration reference (Figure 5.11). Prior to electrochemical testing, all cathodes were de-sodiated by being charged to 1.1 V vs Fc/Fc<sup>+</sup>, rinsed, and then reassembled in a new cell with fresh electrolyte H-CuHCF displays a single, broad oxidation peak centered at 0.64 V, ranging from 0.18 V to 0.90 V (vs Fc/Fc<sup>+</sup>) and two equally prominent reduction peaks at 0.64 V and 0.30 V (vs Fc/Fc<sup>+</sup>). A similar result has been observed for CuHCF under



**Figure 5.10** Cyclic voltammograms at a scan rate of 0.5 mV s<sup>-1</sup> in 1 M Mg(ClO<sub>4</sub>)<sub>2</sub> in PC/EC = 50/50. (a) H-CuHCF. (b) D-CuHCF



**Figure 5.11** CV of H-CuHCF (vs Ag/Ag<sup>+</sup>) in 1 M Mg(ClO<sub>4</sub>)<sub>2</sub> in PC/EC = 50/50 with ferrocene added to calibrate the Ag/Ag<sup>+</sup> pseudo-reference. The Fc/Fc<sup>+</sup> potential was determined to be -0.365 V vs Ag/Ag<sup>+</sup>.



**Figure 5.12** multiple cyclic voltammograms of H- and D-CuHCF at 10 mVs<sup>-1</sup> and 0.5 mVs<sup>-1</sup>. (a) H-CuHCF at 10 mVs<sup>-1</sup> (b) D-CuHCF at 10 mVs<sup>-1</sup> (c)  $1^{st}$  cycle at 0.5 mVs<sup>-1</sup> of H-CuHCF (d)  $1^{st}$  cycle at 0.5 mVs<sup>-1</sup> of D-CuHCF (e)  $2^{st}$  cycle at 0.5 mVs<sup>-1</sup> of H-CuHCF (f)  $2^{st}$  cycle at 0.5 mVs<sup>-1</sup> of D-CuHCF

Al<sup>3+</sup> intercalation [123]. The oxidation and corresponding reduction peaks above 1.0 V for both H- and D-CuHCF are not believed to be related to either Cu or Fe redox. However, as shown in Figure 5.12, the peaks show no degradation upon multiple cv scans at various current densities, indicating it is reversible in nature. Additionally, no electrolyte consumption is observed after extended charge/discharge testing. D-CuHCF (Figure 5.10b) exhibits similar behavior with a single oxidation peak at 0.61 V vs Fc/Fc<sup>+</sup> and two smaller reduction peaks at 0.30 V and 0.46 V vs Fc/Fc<sup>+</sup>, which align with the second oxidation peak of H-CuHCF. Additionally, the normalized, integrated current (mC g<sup>-1</sup>) for D-CuHCF is 43% lower than that of H-CuHCF indicating fewer  $Mg^{2+}$  ions are able to enter the lattice at a scan rate of 0.5 mV s<sup>-1</sup>. The two oxidation peaks for CuHCF may signify that both Fe and Cu undergo reduction/oxidation or that two distinct Fe environments exist. The general electrochemical behavior of CuHCF is known to be more complex than that of other Prussian Blue analogues, as the intercalating ion can influence the activity of  $Cu^{2+}/Cu^+$ . Wessells et al. have reported copper inactivity during Na intercalation [230], while Mizuno et al. demonstrated with ex situ Mössbauer spectroscopy and X-ray absorption near edge structure (XANES) that copper can switch between  $Cu^{2+}/Cu^+$  during  $Mg^{2+}$  intercalation [111]. Also, Mullaliu et al. and others have provided further evidence for the electroactivity of copper in PBAs [254,255]. However, without additional tests, it is not possible to conclusively determine if copper is indeed undergoing redox in our samples given that the specific capacity of our material is below the theoretical capacity of Fe switching (Fe<sup>2+</sup>/Fe<sup>3+</sup>).

Galvanostatic charge discharge tests at various current densities were conducted to investigate the effect of water on the electrochemical charge storage of CuHCF. Ex situ EDX measurements at different states of charge confirmed Mg<sup>2+</sup> intercalation/deintercalation (Figure 5.13). At the lowest current density of 25 mA g<sup>-1</sup>, Hand D-CuHCF deliver reversible specific capacities of 63 and 50 mAh g<sup>-1</sup> respectively (Figure 5.14a) with coulombic efficiencies of 98 %. The capacities are calculated using the entire mass of the cathode coating mixture, not just the active material, and are comparable to both aqueous and nonaqueous CuHCF systems [111,115]. The differential 100







**Figure 5.14** (a) Galvanostatic charge/discharge profiles of H- and D-CuHCF at 25 mA g<sup>-1</sup> in 1 M Mg(ClO<sub>4</sub>)<sub>2</sub> in PC/EC = 50/50. All current densities and capacities are calculated by considering the total mass of the electrode coating. (b) Differential capacity plots of charge/discharge profiles at 25 mA g<sup>-1</sup>. H-CuHCF exhibits two reduction steps, while D-CuHCF only displays a single step. The higher potential redox process observed in H-CuHCF accounts for 25% of its total specific capacity.

capacity plots reveal a contrast in the discharge processes between the two samples. H-CuHCF undergoes a two-step redox process at 0.53/0.42 V and 0.72/0.68 V vs Fc/Fc<sup>+</sup>, whereas D-CuHCF exhibits a single step at 0.56/0.48 V vs Fc/Fc<sup>+</sup> (Figure 5.14b). The oxidation and reduction potentials as determined from the differential capacity are consistent with the CV results (Figure 5.15). As only a single redox pair is observed for D-CuHCF, it can be concluded that the reaction at 0.53/0.42 V for H-CuHCF and 0.56/0.48 V for D-CuHCF corresponds to the  $Fe^{2+}/Fe^{3+}$  switch. The higher potential redox reaction between 0.82 V (vs Fc/Fc<sup>+</sup>) and 0.58 V (vs Fc/Fc<sup>+</sup>) contributes 25% of H-CuHCF's total



**Figure 5.15** Cyclic voltammograms vs differential capacity plots for **(a)** D-CuHCF. **(b)** H-CuHCF. The difference in redox potentials as measured by the two methods range from 1 mV to 102 mV.



**Figure 5.16** Electrochemical and charge storage characterization of H- and D-CuHCF in 1 M Mg(ClO<sub>4</sub>)<sub>2</sub> in PC/EC = 50/50. All current densities and capacities are calculated taking total electrode mass into account. **(a)** Rate capability tests for H- and D- CuHCF. **(b)** Capacity retention of H- and D-CuHCF cathodes over 500 cycles at 300 mA g<sup>-1</sup>. Neither sample experienced any capacity loss after the extended cycling.

capacity and accounts for the loss of capacity upon dehydration. Despite the decrease in capacity upon dehydration the voltage hysteresis' (over potential) of the two samples, which range from 42 to 111 mV, are low for divalent ion insertion and further illustrate the superior Mg<sup>2+</sup> kinetics of CuHCF [115].

Rate capability tests were performed at current densities of 25, 45, 65, 85, 100, and 200 mAh g<sup>-1</sup> (Figure 5.16a). Both H- and D-CuHCF display good performance, retaining over 65% of their initial capacity when the current density was increased from 25 to 200 mA g<sup>-1</sup>. Upon returning to 25 mA g<sup>-1</sup>, both samples recover 100% of their initial capacity. The corresponding discharge profiles are shown in Figure 5.17. Cycle lifetimes were examined over 500 cycles at 300 mA g<sup>-1</sup> (Figure 5.16b). Neither H- or D-CuHCF



**Figure 5.17** Gavanostatic discharge profiles at different current densities in 1 M  $Mg(CIO_4)_2$  in PC/EC = 50/50 to determine the rate capabilities. **(a)** Discharge profiles of H-CuHCF. **(b)** Discharge profiles of D- CuHCF.

experienced any capacity fading over the extended testing, while delivering reversible capacity of 38 and 35 mAh g<sup>-1</sup> with coulombic efficiencies of 100% and 94%, respectively. The increase in reversible capacity of both samples after 500 charge/discharge cycles is thought to result from the intercalation of electrolyte into the lattice, causing the cathodes to slowly become wetted. Similar results have been reported for other PBA systems [256].

To further examine the  $Mg^{2+}$  insertion/extraction reaction kinetics, cyclic voltammograms at varying sweep rates from 10 to 50 mVs<sup>-1</sup> were collected (Figure 5.18 a, d). The peak cathodic and anodic currents each obey a power-law relationship with respect to scan rate (v):

$$i = av^b \tag{5.1}$$

where a and b are adjustable parameters. The exponential parameter b reflects the rate limiting step in the electrochemical reaction. A value of b = 0.5 represents a diffusion-controlled process, while b = 1.0 suggests non-faradic (capacitive) behavior [257]. The b parameter for each case was determined from the slopes of the logarithmic plots shown in Figure 5.18b and Figure 5.18e. b values of 0.64 and 0.59 were determined for the cathodic and anodic reactions of H-CuHCF respectively, while values of 0.57 and 0.51 were determined for D-CuHCF's cathodic and anodic reactions, respectively. All b values are close to 0.5 indicating a diffusion-limiting process for both samples, with H-CuHCF displaying slightly more pseudocapactive behavior than D-CuHCF.



**Figure 5.18** (a,d) Cyclic voltammograms of H- and D-CuHCF at scan rates from 10 to  $50 \text{ mV s}^{-1}$  in 1 M Mg(ClO<sub>4</sub>)<sub>2</sub> in PC/EC = 50/50. (b,e) the corresponding log (peak current density) vs log (sweep rate) plots used to calculate the b coefficients. (c, f) the corresponding peak current density vs square root of the scan rate plots used to estimate Mg<sup>2+</sup> diffusion coefficients.

Diffusion coefficients were estimated by the Randles-Sevcik equation, fitted to the linear plot of peak current versus square root of the scan rate shown in Figure 5.18c and

Figure 5.18f, which models diffusion limited quasi-reversible reactions [206]:

$$i_{peak} = 0.4463 x \sqrt{\frac{n^3 F^3}{RT}} x \sqrt{D} x C_o x \sqrt{\nu}$$
(5.2)

where  $i_p$  is the peak current (A), n is the number of electrons transferred in the reaction, F is Faraday's constant, R is the ideal gas constant, T is temperature (K), D is the diffusion 106 coefficient (cm<sup>2</sup> sec<sup>-1</sup>), C<sub>0</sub> is the concentration of active sites (mol cm<sup>-3</sup>), and v is the cyclic voltammogram sweep rate. C<sub>0</sub> was estimated from the specific capacitance and density of the material. Diffusion coefficients for the oxidation (D<sub>ox</sub>) and reduction (D<sub>red</sub>) reactions of H-CuHCF were estimated to be 4.8 x 10<sup>-10</sup> and 4.1 x 10<sup>-10</sup> cm<sup>2</sup> sec<sup>-1</sup> respectively, and 2.5 x 10<sup>-10</sup> and 1.8 x 10<sup>-10</sup> cm<sup>2</sup> sec<sup>-1</sup> for D-CuHCF respectively, which are on the order of other nonaqueous PBA systems [77]. The similar Mg<sup>2+</sup> diffusion kinetics and rate capability of both the hydrated and dehydrated samples highlights the importance of the shared structural properties of CuHCF, including its open framework and mechanical stability. Neither H- or D-CuHCF display any degradation after undergoing rate or lifetime tests, while delivering reversible capacities of 63 and 50 mAh g<sup>-1</sup> at 25 mA g<sup>-1</sup>, respectively. The increase in capacity for H-CuHCF is attributed to the accessibility of a second redox step that accounts for 25% of its total capacity (16 mAh g<sup>-1</sup>) at 25 mA g<sup>-1</sup>.

To better understand the role of water during charging/discharging, ex situ FTIR spectra of H-CuHCF were collected (Figure 5.19). The large absorption peak at 1763 cm<sup>-1</sup> corresponds to the C=O stretching frequency of ethylene carbonate [258], confirming the intercalation of electrolyte into the CuHCF lattice. The zeolitic and coordinated water peak at 1628 cm<sup>-1</sup> maintains a constant intensity between the fully charged and fully discharged states, indicating that water does not accompany Mg<sup>2+</sup> during intercalation/deintercalation, but instead remains within the lattice. Based on this stability, it is proposed that the internal water is predominantly coordinated to the CuHCF framework at the 24e site. The second redox reaction and improved charge storage 107



**Figure 5.19** Ex situ FTIR analysis of H-CuHCF. The interstitial and zeolitic water peak at 1628 cm<sup>-1</sup> does not change between fully charge and fully discharged, demonstrating the water does not leave the lattice.

capacity of H-CuHCF are believed to be due to electrostatic shielding provided by the static coordinated and zeolitic water, which allows for the B lattice sites with dangling Cu atoms to become thermodynamically accessible [115]. The presence of water in the lattice has been proposed to have similar effects for PBAs, as well as other magnesium ion cathodes, such as: layered MoO<sub>2</sub> [245], and V<sub>2</sub>O<sub>5</sub> [246].

# 5.6 Conclusion:

The charge storage capacities of hydrated and dehydrated CuHCF in non-aqueous electrolytes have been investigated by characterizing the structural and electrochemical properties of hydrated and dehydrated CuHCF. Both hydrated and dehydrated CuHCF show reversible Mg<sup>2+</sup> intercalation, and zeolitic and coordinated water content was shown to increase measured charge storage capacity by approximately 25%. FTIR and TGA analysis show that thermal treatment of the bare CuHCF powder at 100 °C effectively removes 63% of the zeolitic and coordinated water molecules, while prepared H-CuHCF electrodes are able to retain their water effectively during the curing process. This result is believed to be due to the presence of the PVDF binder, which helps keep water in the H-CuHCF lattice. Benefiting from the stable structure and large interstitial spacing of the underlying CuHCF framework, both the hydrated and dehydrated materials exhibit excellent rate and cycle lifetime performances, neither of which show any loss of capacity after 500 cycles at 300 mA g<sup>-1</sup>. However, by maintaining its zeolitic and coordinated water, H-CuHCF achieves a 25% increase in storage capacity. Ex situ FTIR reveals that water does not accompany Mg<sup>2+</sup> ions during intercalation/deintercalation. We propose that the water plays a supporting role within the lattice, providing partial electrostatic screening of the divalent Mg ions, while also allowing a new redox transition to become thermodynamically accessible. The presence of a second redox peak in H-CuHCF accounts for the difference in storage capacity between H-CuHCF and D-CuHCF.

#### **5.7 Additional Commentary on Published Work**

**Kuperman N**, Cairns A, Goncher G, Solanki R. Structural water enhanced intercalation of magnesium ions in copper hexacyanoferrate nonaqueous batteries. Electrochimica Acta 2020;362:137077. <u>https://doi.org/10.1016/j.electacta.2020.137077</u>. [238]

The studies presented in this chapter were undertaken to:

- Develop non-lithium ion based systems utilizing PBA cathodes, with a particular focus on divalent ion systems.
- 2. Determine if maintaining coordinated and zeolitic water improved the magnesium ion storage properties of copper hexacyanoferrate in a nonaqueous electrolyte.

The results obtained in this study helped to accomplish these goals by expanding our knowledge of the effects of coordinated and zeolitic water in the battery system consisting of a Cu[Fe(CN)<sub>6</sub>] cathode with a Mg<sup>+2</sup> cation in a non-aqueous solvent (propylene carbonate and ethylene carbonate mixture). Mizuno et al. demonstrated reversible intercalation of Mg into CuHCF in an aqueous electrolyte and reported a reversible specific capacity of 50 mAh g<sup>-1</sup> [111]. The specific capacity of CuHCF in the completely nonaqueous systems reported in this work was smaller than Mizuno's value, as expected, a consequence of different ionic mobilities in the electrolyte and ionic diffusion in the PBA lattice. However, by retaining coordinated water in CuHCF, specific 110

capacities for nonaqueous electrolytes were consistent with those reported by Mizuno. The benefit of nonaqueous electrolytes is the ability to use metallic Mg anodes, which can provide significant increases in energy density. In general, Mg metal is not volatile in air which reduces potential catastrophic failures, and Mg is relatively abundant (7th most abundant element in the Earth's crust).

## Chapter 6.

# Manganese-Nickel Hexacyanoferrate and its Application as a Cathode Material for Nonaqueous Potassium Ion Batteries

This chapter examines manganese-nickel hexacyanoferrate as a cathode material for nonaqueous potassium ion batteries (PIBs). Temporary closures of crucial facilities due to the COVID-19 pandemic have prolonged the completion of this study and thus a manuscript is now being prepared for submission. All experimental data have been collected and analyzed except for scanning electron microscopy, energy dispersive x-ray spectroscopy and inductively coupled plasma mass spectroscopy (ICP-MS). These final measurements will provide information on particle size and morphology, elemental distribution, and elemental composition of materials. In particular, particle size could inform the analyses of ionic diffusion and rate capability.

The following work is presented in its current form and additional comments on the potential impact of the uncollected data is at the end.

# 6.1 Introduction

This study examines manganese-nickel hexacyanoferrate (MnNiCHF) as a cathode material for nonaqueous potassium ion batteries. Pure nickel hexacyanoferrate has the advantage of being structurally stable during discharge, but suffers from low specific capacities due to the redox inactivity of Ni. Pure manganese hexacyanoferrate has a high theoretical capacity as Mn is redox active, however Jahn-Teller distortions during charging and discharging cause significant capacity loss over time [153,259–261]. Figure 6.1 presents a schematic representation of NaMn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>].



**Figure 6.1** Schematic of Na<sub>2</sub>Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>].

The goal of this study was to determine if the introduction of both Ni and Mn into a mixed-metal hexacyanoferrate could provide improved capacity, compared to either NiHCF or MnHCF, by combining the crystal stability provided by Ni atoms with the favorable redox properties provided by Mn atoms.

The materials chosen for examination are Na<sub>2</sub>Ni[Fe(CN)<sub>6</sub>], Na<sub>2</sub>Mn[Fe(CN)<sub>6</sub>], Na<sub>2</sub>Mn<sub>0.50</sub>Ni<sub>0.50</sub>[Fe(CN)<sub>6</sub>] and Na<sub>2</sub>Mn<sub>0.25</sub>Ni<sub>0.75</sub>[Fe(CN)<sub>6</sub>]. The latter two materials possess the same cubic crystal structure as NiHCF, eliminating the impact of crystalline phase. Na<sub>2</sub>Mn[Fe(CN)<sub>6</sub>] crystallized in a monoclinic structure, however the impact of increasing Mn concentrations occurs prior to the change in phase, allowing for trends independent of structure to be identified.

## 6.2 Methods

## 6.2.1 Synthesis:

Nickel hexacyanoferrate was synthesized via coprecipitation similar to our previous work, with slight modification [221]. Briefly, 40 mM of NiCl<sub>2</sub>·6H<sub>2</sub>O was dissolved in 80 mL of deionized (DI) water (solution A), and 20 mM of Na<sub>4</sub>Fe(CN)<sub>6</sub> was dissolved separately in 80 mL of DI water (solution B). Solutions A and B were simultaneously added dropwise into 40mL NaCl (5M aq) under constant stirring and maintained at 60 °C for two hours. The resulting precipitate was collected, washed via centrifugation with DI water followed by a final wash with ethanol, and allowed to dry in air. After air drying, the resulting powder was annealed at 100 °C under vacuum for two hours and allowed to cool

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slowly. The same procedure was followed to synthesize the mixed nickel manganese and pure manganese hexacyanoferrate powders, except that the ratio of metal chloride salts varied depending on the sample. The Ni:Mn ratios were: 1:0, 3:1, 1:1, and 0:1 denoted as NiHCF, MnNiHCF-1, MnNiHCF-2, and MnHCF respectively.

## **6.2.2** Material Characterization:

The crystal structure of each sample was characterized using powder X-ray diffraction (XRD) performed on a Rigaku Ultima IV X-ray diffractometer with Cu K $\alpha$  radiation ( $\lambda$ =1.54056 Å). Indexing and structure refinement were conducted using the Fullprof crystallographic suite [215,247]. Thermal and water content analysis was performed using a thermogravimetric analyzer (TGA, Mettler TGA-50) from 50 to 300 °C at a heating rate of 5 °C min<sup>-1</sup> under flowing N<sub>2</sub>. Fourier transform infrared spectroscopy (FTIR, Thermo Scientific Nicolet iS10 FTIR equipped with diamond ATR) in the range of 600 – 3800 cm<sup>-1</sup> was used to probe the chemical environment of the cyanide ligand and determine the oxidation states of the transition metals. FTIR in the range of 90 – 690 cm<sup>-1</sup> was performed on a Thermo Scientific Nicolette 6700 equipped with a DTGS detector to probe the metal-carbon and metal-nitrogen bonding.

## 6.2.3 Electrochemical Measurements:

Cathodes were prepared by coating a slurry of a Na<sub>x</sub>Mn<sub>y</sub>Ni<sub>1-y</sub>[Fe(CN)<sub>6</sub>] powder, polyvinylidene fluoride (PVDF), multi-walled carbon nanotubes, and activated carbon in

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the ratio of 80:9:9:2, respectively by weight in N-methyl-2-pyrolidone (NMP) onto carbon paper. The carbon paper was cleaned with ethanol and dried prior to use. Coated electrodes were annealed for two hours at 100 °C under vacuum prior to use. All electrochemical measurements were performed using a Gamry reference-600 potentiostat in a three-electrode setup. In general, cells consisted of the respective cathode, a carbon rod counter electrode, an Ag/Ag<sup>+</sup> in propylene carbonate reference electrode, and an electrolyte of saturated potassium hexafluorophosphate (sat KPF<sub>6</sub>) in a mixture of propylene carbonate (PC) and ethylene carbonate (EC) [PC/EC = 50/50 by volume]. All reference electrodes were calibrated against the Fc/Fc<sup>+</sup> redox couple.

## 6.3 Results

The XRD patterns of the as synthesized powders are shown in Figure 6.2a. NiHCF is indexed to the well-known PBA cubic structure with lattice parameter 10.20 Å. Substitution of Mn for Ni causes an expansion of the lattice, observed as a downward shift in 2 $\Theta$  (Figure 6.2b). This is a consequence of the larger radius of high spin, octahedrally crystallized coordinated, Mn<sup>2+</sup> (97 pm) compared to the octahedrally coordinated Ni<sup>2+</sup> (83 pm) [232]. MnNiHCF-1, and MnNiHCF-2 are indexed to cubic systems with lattice parameters 10.27 Å, and 10.33 Å respectively. The XRD patterns for the mixed metal samples confirm that each formed a single phase, incorporating both Mn and Ni, rather than mixtures of NiHCF and MnHCF. Pure MnHCF shows a monoclinic structure with lattice parameters a = 10.54 Å, b = 7.47 Å, c = 7.41 Å, and  $\beta$  = 91.83°. MnHCF with high Na



**Figure 6.2** (a) XRD profile for the as-synthesized, unannealed,  $Na_2Mn_xNi_{1-x}[Fe(CN)_6]$  powders. NiHCF, MnNiHCF-2, and MnNiHCF-2 all crystallized into a cubic structure, and MnHCF crystallized into a monoclinic structure. (b) (200) reflection for as synthesized samples. The decreasing 2 $\Theta$  indicates an increasing lattice parameter with increasing Mn concentration.



**Figure 6.3** (200) reflection for the as-synthesized (dotted lines) and the annealed (solid lines) samples

concentrations is known to undergo the observed monoclinic distortion [251,262]. XRD profiles of the annealed samples show increases in 2 $\Theta$  of the largest diffraction peak, which corresponds to the (200) reflection, indicating a contraction of the lattice (figure 6.3). Similar phenomena have been reported for PBAs upon the removal of interstitial and coordinated water [149]. The pre and post anneal lattice parameters presented in table 6.1.

	As synthesized	Annealed 100° C
NiHCF	a = b = c = 10.20 Å	a = b = c = 10.21 Å
	$\alpha = \beta = \gamma = 90^{\circ}$	$\alpha = \beta = \gamma = 90^{\circ}$
MnNiHCF-1	a = b = c = 10.27 Å	a = b = c = 10.25 Å
	$\alpha = \beta = \gamma = 90^{\circ}$	$\alpha = \beta = \gamma = 90^{\circ}$
MnNiHCF-2	a = b = c = 10.33 Å	a = b = c = 10.32 Å
	$\alpha = \beta = \gamma = 90^{\circ}$	$\alpha = \beta = \gamma = 90^{\circ}$
MnHCF	a = 10.54 Å, b = 7.47 Å, c = 7.41 Å	a = 10.51 Å, b = 7.45 Å, c = 7.38 Å
	$\alpha = \gamma = 90^{\circ}, \beta = 91.83^{\circ}$	$\alpha = \gamma = 90^{\circ}, \beta = 92.01^{\circ}$



**Figure 6.4** Thermogravimetric curves for as-synthesized  $Na_2Mn_xNi_{1-x}[Fe(CN)_6]$  samples. The zeolitic water contentment for each sample increases with Mn concentration, while the percentage of coordinated water for each sample is 9%.

Thermogravimetric analysis was carried out to study the water content of the Na<sub>2</sub>Mn<sub>x</sub>Ni<sub>1-x</sub>HCF samples. Figure 6.4 displays the TGA spectra for the as-synthesized samples, each exhibiting a multistep dehydration process. The two mass loss steps occurring between 50 °C and 210 °C are associated with the removal of water molecules from distinct lattice locations: the first corresponds to removal of zeolitic water and the second to the removal of coordinated water [263]. Interestingly, the amount of coordinated water is relatively consistent across all samples but the concentration of

zeolitic water decreases with increasing manganese. After annealing, all samples show a decrease in zeolitic water content but no loss in coordinated water. TGA data is summarized in Table 6.2.

FTIR spectroscopy was applied to examine the effects of substituting Mn, for Ni, on the bonding characteristics of the resulting manganese-nickel hexacyanoferrate. The vibrational properties of the cyanide in a PBA are dependent on the coordinated metal atoms, their respective oxidation state(s) and electronegativities, providing individual signatures for each material [264–266]. Figure 6.5 displays spectra for the as-prepared samples.

	As synthesized	Annealed 100° C
NiHCF	Zeolitic: 8%	Zeolitic: 5%
	Coordinated: 9%	Coordinated: 8%
MnNiHCF-1	Zeolitic: 13%	Zeolitic: 8%
	Coordinated: 9%	Coordinated: 9%
MnNiHCF-2	Zeolitic: 15%	Zeolitic: 11%
	Coordinated: 9%	Coordinated: 9%
MnHCF	Zeolitic: 18%	Zeolitic: 10%
	Coordinated: 9%	Coordinated: 9%

**Table 6.2**Summary of zeolitic and coordinated water content as determined by<br/>thermogravimetric analysis.

The strong absorption band in the range of 2000 - 2080 cm<sup>-1</sup> is characteristic to the cyanide stretching frequency, v(CN), of M<sup>2+</sup>-NC-Fe<sup>2+</sup> (M = Ni, Mn) [267–270]. Substitution of Mn<sup>2+</sup> ( $\sigma_{Mn} = Z/r^2 = 2.9$ ) for Ni<sup>2+</sup> ( $\sigma_{Ni} = Z/r^2 = 4.2$ ) lowers the effective polarizing power ( $\sigma_{eff} = x^* \sigma_{Mn} + (1-x)^* \sigma_{Ni}$ ) of the N-coordinated metals, inducing a redistribution of the electron density across the cyanide towards the carbon end of the ligand [84]. This shift causes the CN triple bond to weaken, observed as a linear decrease in v(C=N) with respect to Mn concentration.

The broad band centered at 3350 cm<sup>-1</sup> corresponds to the O-H stretching frequency of free surface water, while the sharp peak at 1610 cm<sup>-1</sup> and shoulder at 1650 cm<sup>-1</sup> are characteristic of zeolitic water and coordinated water respectively [251]. With increasing Mn, each water peak decreases in intensity, mirroring the TGA data and further highlighting the impact of Mn on the quality of the as-synthesized material. FTIR spectra of the annealed samples confirms the successful removal of the majority of surface water and partial removal of zeolitic water (Figure 6.6).

FTIR spectra in the far IR region were collected to directly probe the local environment around the carbon end of the cyanide bond (Figure 6.7). The band near 600 cm<sup>-1</sup> is assigned to the Fe-C stretching frequency, v(Fe-C) [271]. With increasing Mn concentrations, the Fe-C band shifts to higher wavenumbers indicating a shortening and strengthening of the Fe-C bond. Both v(Fe-C) and v(C=N) exhibit a linear relationship with the effective polarizating power of the N-coordinated metals as shown in Figure 6.8.



**Figure 6.5** a) FTIR of the as-synthesized Na<sub>2</sub>Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>]. b) v(C=N) of the as-synthesized samples. The downward shift in v(C=N) with increasing Mn concentration indicates a weakening of the cyanide bond.



**Figure 6.6** FTIR spectra of the 100  $^{\circ}$ C annealed samples of Na<sub>2</sub>Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>].



**Figure 6.7** a) Far IR FTIR spectra for the as-synthesized Na<sub>2</sub>Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>] samples. b) v(Fe-C) of the as-synthesized samples. The upward shift in v(Fe-C) with increasing Mn concentration indicates a strengthening of the Fe-C bond.



**Figure 6.8** Relationships between the effective polarizing power of the nitrogen coordinated metals and the stretching frequencies for v(C=N) and v(Fe-C).  $\sigma_{eff}$  decreases with increasing Mn concentration, which in a decrease in v(C=N) and increase in v(Fe-C). These trends are indicative of a weakening of the cyanide bond and a strengthening of the iron-carbon bond.

**SEM + EDS Data:** These results are pending.

ICPMS Data: These results are pending.

The electrochemical performances of the Mn<sub>x</sub>Ni<sub>1-x</sub>HCF samples were examined by galvanic charge discharge and cyclic voltammetry. All measurements were conducted using a three-electrode configuration in sat KPF<sub>6</sub> in PC and EC in a 1-to-1 ratio by volume and referenced to the Fc/Fc<sup>+</sup> redox couple. As indicated by Figure 6.9 the Fe<sup>3+</sup>/Fe<sup>2+</sup> discharge potential is linearly proportional to the Mn concentration as well as the ironcarbon stretching frequency, with NiHCF (0.35 V vs Fc/Fc<sup>+</sup>) < MnNiHCF-1 (0.40 V vs Fc/Fc<sup>+</sup>) < MnNiHCF-2 (0.42 V vs Fc/Fc<sup>+</sup>) < MnHCF (0.48 V vs Fc/Fc<sup>+</sup>). Other reports have shown similar behavior, with the iron redox potential varying linearly with respect to changing the ratio of two N-coordinated transition metals [93,153]. Figure 6.10a-d compares the initial charge discharge profiles at 25 mAg<sup>-1</sup> of the mixed metal samples as well as the homogeneous NiHCF and MnHCF. Specific capacities of the Ni containing samples increase with Mn incorporation, with NiHCF, MnNiHCF-1 and MnNiHCF-2 delivering capacities of 80, 103, and 110 mAhg<sup>-1</sup> respectively. A decrease in the reversible capacity of pure MnHCF to 105 mAhg<sup>-1</sup> is observed, despite its conformity to the relationship between Fe<sup>2+</sup>/Fe<sup>3+</sup> redox potential and Mn concentration. The increase in the specific capacities of MnNiHCF-1 and MnNiHCF-2 is ascribed to the substitution of the electroactive Mn for the electrochemically inactive Ni. However, the decreased capacity and increased Fe<sup>2+</sup>/Fe<sup>3+</sup> redox potential of MnHCF highlights the important role both Ni



**Figure 6.9** (a) Plot of  $Fe^{3+}/Fe^{2+}$  discharge potential verses percent Mn. (b) Plot of  $Fe^{3+}/Fe^{2+}$  discharge potential verses v(Fe-C)

and Mn have on modulating the electrochemical and physical properties of the resulting and increased Fe<sup>2+</sup>/Fe<sup>3+</sup> redox potential of MnHCF highlights the important role both Ni and Mn have on modulating the electrochemical and physical properties of the resulting material.

Rate capability tests for each sample were conducted at 45, 65, 85, 100, and 200 mAg<sup>-1</sup> (Figure 6.10e). Figure 6.10f compares the normalized capacity ( $Q/Q_0$ ) of the samples as a function of current density, where Q is the capacity at different current densities and  $Q_0$  is the capacity at 25 mAg-1. NiHCF, MnNiHCF-1 and MnNiHCF-2 each exhibit excellent capacity retention at increased current densities, respectively delivering 69, 85, and 90 mAhg<sup>-1</sup> accounting for 85%, 83%, and 81% of their initial capacities at 200 mAg<sup>-1</sup>. Additionally, all Ni contain samples recovered 100% of their initial capacity


**Figure 6.10** Galvanostatic charge discharge, at 25 mAg<sup>-1</sup>, of **a**) NiHCF, **b**) MnNiHCF-1, **c**) MnNiHCF-2, and **d**) MnHCF. **e**) Rate data for  $Na_2Mn_xNi_{1-x}[Fe(CN)_6]$ . **f**) Normalized capacity vs current density for  $Na_2Mn_xNi_{1-x}[Fe(CN)_6]$ . The rate capability of a material is inversely related to the percentage of Mn. **g**) Cycle lifetimes of  $Na_2Mn_xNi_{1-x}[Fe(CN)_6]$ . Each cathode displays excellent performance over extended cycling at 300 mAg<sup>-1</sup>.

upon returning to 25 mAg<sup>-1</sup>. The slight drop in rate performance for MnNiHCF-1 and MnNiHCF-2 exposes the adverse effect of Mn on the resulting materials rate capability. Pure MnHCF experiences a rapid decrease in capacity retention with increased current densities, delivering only 73 mAhg<sup>-1</sup> at 200 mAg<sup>-1</sup> (70 % of its initial capacity), and recovering only 90% of its initial capacity at 25 mAg<sup>-1</sup>. Cycling stability of each material was examined over 300 cycles at 300 mAg<sup>-1</sup> (Figure 6.10g). Capacity retention was 99% for NiHCF, 98% for MnNiHCF-1, 97% for MnNiHCF-2, and 100% for MnHCF. These performances underscore the reversibility of each material at high current densities.

Cyclic voltammograms at sweep rates between 0.1 and 1 mVs<sup>-1</sup> were carried out to gain further insight into K<sup>+</sup> reaction kinetics of each sample. At 0.1 mVs<sup>-1</sup>, each nickel containing sample displays a single prominent redox couple associated with the Fe<sup>2+</sup>/Fe<sup>3+</sup> reaction, with half potentials of 0.36, 0.41, 0.43 V vs Fc/Fc+ for NiHCF, MnNiHCF-1, and MnNiHCF-2 respectively (Figure 6.11a-c). The manganese redox reaction appears as shoulders in the MnNiHCF-1 (0.47 V vs Fc/Fc<sup>+</sup>) and MnNiHCF-2 (0.55 V vs Fc/Fc<sup>+</sup>) CV curves. Two oxidation/reduction peaks are present in the MnHCF voltammogram, with the reaction half potentials at 0.52 V vs Fc/Fc<sup>+</sup> and 0.71 V vs Fc/Fc<sup>+</sup> corresponding to the Fe<sup>2+</sup>/Fe<sup>3+</sup> and Mn<sup>2+</sup>/Mn<sup>3+</sup> redox reactions, respectively (Figure 6.11d). Figure 6.12a-d shows the cyclic voltammograms for each sample at various scan rates. The relationship between peak current and sweep rate for a reversible or quasi-reversible diffusion controlled electrochemical reaction is described by the Randles-Sevcik equation (equation 6.1) [206]:

$$i_{peak} = 0.4463 x \sqrt{\frac{n^3 F^3}{RT}} x \sqrt{D} x C_o x \sqrt{\nu}$$
(6.1)



**Figure 6.11** Cyclic voltammograms at 0.1 mV s<sup>-1</sup> of **a)** NiHCF, **b)** MnNiHCF-1, **c)** MnNiHCF-2, and **d)** MnHCF



**Figure 6.12** Cyclic voltammograms from  $0.1 - 1.0 \text{ mV s}^{-1}$  and the corresponding peak current vs (scan rate)<sup>1/2</sup> for (a,e) NiHCF, (b,f) MnNiHCF-1, (c,g) MnNiHCF-2, and (d,h) MnHCF.

where  $i_p$  is the peak current (A), n is the number of electrons transferred in the reaction, F is Faraday's constant, R is the ideal gas constant, T is temperature (K), D is the diffusion coefficient (cm<sup>2</sup> sec<sup>-1</sup>), C<sub>0</sub> is the concentration of active sites (mol cm<sup>-3</sup>), and v is the cyclic voltammogram sweep rate. C<sub>0</sub> for each material was estimated from the specific capacity of the materials. Using the slopes from the lines of best fit of the peak current (I<sub>peak</sub>) versus the square root of the scan rate (v<sup>1/2</sup>), diffusion coefficients for the Fe<sup>2+</sup>/Fe<sup>3+</sup> oxidation/reduction reactions (Figure 6.12e-h). Table 6.3 presents the calculated diffusion coefficients. The drop in the K<sup>+</sup> diffusion for MnNiHCF-2 as well as MnHCF further demonstrates the adverse effect/impact of Mn on K<sup>+</sup> mobility independent of any structural shifts.

**Table 6.3**Slopes determined from best fit lines in Figure 6.2 e-h and the calculatedanodic and cathode K<sup>+</sup> diffusion coefficients for the  $Fe^{2+}/Fe^{3+}$  redox reaction of $Mn_xNi_{1-x}[Fe(CN)6]$ 

Sample	Anodic slope	Cathodic slope	Anodic diffusion coeff.	Cathodic diffusion coeff.
	$\frac{mA \ s^{1/2}}{mg \ mV^{1/2}}$	$\frac{mA s^{1/2}}{mg mV^{1/2}}$	$\frac{cm^2}{s}$	$\frac{cm^2}{s}$
NiHCF	-8.86 x 10 <sup>-4</sup>	8.95 x 10 <sup>-4</sup>	8.71 x 10 <sup>-6</sup>	8.88 x 10 <sup>-6</sup>
MnNiHCF-1	-1.25 x 10 <sup>-4</sup>	1.14 x 10 <sup>-4</sup>	8.92 x 10 <sup>-6</sup>	7.40 x 10 <sup>-6</sup>
MnNiHCF-2	-1.48 x 10 <sup>-4</sup>	1.28 x 10 <sup>-4</sup>	7.16 x 10 <sup>-6</sup>	5.35 x 10 <sup>-6</sup>
MnHCF	-1.65 x 10 <sup>-4</sup>	8.49 x 10 <sup>-4</sup>	3.79 x 10 <sup>-8</sup>	9.98 x 10 <sup>-7</sup>

## 6.4 Discussion

The goal of this study was to determine if the introduction of both Ni and Mn into a mixed-metal hexacyanoferrate could provide improved capacity, compared to either NiHCF or MnHCF, by combining the crystal stability provided by Ni atoms with the favorable redox properties provided by Mn atoms.

Of the materials examined in this work, Mn<sub>0.50</sub>Ni<sub>0.50</sub>[Fe(CN)<sub>6</sub>] delivers the highest specific capacity (110 mAhg<sup>-1</sup> at 25 mAg<sup>-1</sup>) without significant sacrifice in rate performance. This is attributed to the synergetic effects of manganese and nickel, with manganese providing addition storage capacity due to the Mn<sup>2+</sup>/Mn<sup>3+</sup> transition and nickel stabilizing the overall crystal structure and in particular the Mn-N-C-Fe chain. The addition of Mn increases the specific capacity of MnNiHCF-2 by 25% compared to pure NiHCF. The stabilization offered by nickel enables fast K<sup>+</sup> diffusion and accounts for the good rate performance of MnNiHCF-2 Both mixed manganese-nickel hexacyanoferrate samples displayed superior rate capability and cycle lifetimes compared to pure MnHCF. This result is consistent with the initial hypothesis that replacing Mn with Ni in the HCF lattice would improve electrochemical stability.

For all samples, a linear relationship between the specific capacity vs log (current density) of the sample is observed (Figure 6.13). By extrapolating the best fit curves, it is possible to obtain an approximation of the maximum achievable capacity as the current



**Figure 6.13** Specific capacity vs. Log (current density) of Na<sub>2</sub>Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>]. The slopes provide a quantitative value related to the rate capability of the different materials. A larger slope corresponds to worse rate performance. By extrapolating the best fit lines to the y-intercept (zero current), a theoretical zero-current capacity can be obtained. At zero current, MnHCF has the highest theoretical capacity followed by MnNiHCF-2, MnNiHCF-1, and NiHCF, respectively.

approaches zero. These results differ from the 25 mAg<sup>-1</sup> charge/discharge capacities, with MnHCF having the largest low-current capacity followed by MnNiHCF-2, MnNiHCF-1, and lastly NiHCF. This data supports the conclusion that pure MnHCF has a lower capacity than MnNiHCF-2, at 25 mAg<sup>-1</sup>, due to resistance to diffusion of the potassium cation.

In general, changing the ratio of Mn and Ni concentrations had three major effects

on electrochemical performance:

For all samples that contain Ni, storage capacity increases with increasing Mn concentration. However, the capacity of pure MnHCF is lower than MnNiHCF-2.

1) Redox potential increases with increasing Mn concentration

2) Diffusion rates of K<sup>+</sup> decrease as Mn concentration increases

The first trend is attributed to the increase in redox active elements in the hexacyanoferrate lattice.

The second trend can be attributed to the modulation of the electron density across the cyanide by adjusting the effective polarization of the nitrogen coordinated metal ( $\sigma_{eff} = x^* \sigma_{Mn} + (1-x)^* \sigma_{Ni}$ ). As the concentration of Mn is increased the value of  $\sigma_{eff}$ decreases. This results in an increase in the electron density at the carbon-Fe end of the cyanide, causing an increase in the electrical potential of the Fe [93].

Analysis of the reasons underlying the third trend will depend upon the outstanding SEM data, which will provide information on particle size. Particle size has been shown to influence the diffusion kinetics of PBAs [108,272].

6.5 Additional Commentary on Manganese-Nickel Hexacyanoferrate and its Application as a Cathode Material for Nonaqueous Potassium Ion Batteries

The studies presented in this dissertation were undertaken to:

- a) Identify novel battery systems that extend beyond lithium and sodium chemistries, and
- b) Provide further insights into the relationship between the metals in mixed metal hexacyanoferrates and the resulting energy storage properties.

The results obtained in this study helped to achieve these goals by:

- Examining, for the first time, the combination of Ni<sub>0.75</sub>Mn<sub>0.25</sub>[Fe(CN)<sub>6</sub>] as a cathode and K<sup>+</sup> as the electrolytic cation in a non-aqueous solvent (propylene carbonate and ethylene carbonate mixture), and
- 2) Examining the effects of the Ni/Mn ratio in the battery system described above.

A synergistic effect between Mn and Ni on the electrochemical properties of the mixedmetal hexacyanoferrate  $Na_2Mn_xNi_{1-x}[Fe(CN)_6]$  was demonstrated. An inverse relationship between rate capability and storage capacity was observed, with  $Mn_{0.50}Ni_{0.50}[Fe(CN)_6]$ offering optimal pairing of storage capacity and diffusion kinetics.

#### Chapter 7.

#### Calculating Electron Density Distribution in Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>]

The experimental IR and electrochemical data presented in chapter 6 suggest that the specific capacity and redox potential of  $Mn_xNi_{1-x}[Fe(CN)_6]$  compounds increase as the electron density across the Fe-C-N-M' chain is drawn towards the Fe-C end. Substituting nitrogen-coordinated Mn for nitrogen-coordinated Ni causes a decrease in stretching frequency (v) of the C=N bond, consistent with bond weakening, and an increase in v of the Fe-C bond, consistent with increases in bond strength and electron density. These findings suggest a shift in average electron density away from the nitrogen-bonded transition metal and towards the iron-carbon bond. This is shown schematically as:

 $Fe - C \equiv N - Ni$ 

$$Fe \leftarrow C \leq N \leftarrow Mn$$

in which the arrows indicate the direction of shifts in electron density as Mn replaces Ni. Density functional theory (DFT) calculations were conducted to further probe the relationship between the Mn concentration in  $Mn_xNi_{1-x}[Fe(CN)_6]$  and: (a) the electron density of the Fe, and (b) the Fe-C bond length.

Traditionally, the ground state electronic structure of a system can be determined by solving the non-relativistic, time independent Schrodinger equation 7.1:

$$\left[-\frac{\hbar^2}{2m}\sum_i \nabla_i^2 + \sum_i V(\boldsymbol{r}_i) + \sum_i \sum_{i,\neq j} U(\boldsymbol{r}_i, \boldsymbol{r}_j)\right] \Psi(\boldsymbol{r}_1, \dots, \boldsymbol{r}_N) = E\Psi(\boldsymbol{r}_1, \dots, \boldsymbol{r}_N)$$
(7.1)

where  $\nabla_i^2$  is the electron kinetic energy, V(r<sub>i</sub>) is the potential energy due to electronnuclei interactions, U(r<sub>i</sub>,r<sub>j</sub>) is the potential energy term due to electron-electron interactions, and E is the energy of the system. In principal, all information about a system can be obtained by solving the many-body Schrodinger equation. However, a closed form analytical solution cannot be written for systems other than hydrogen, and numerical solutions are limited to systems with N ≤ 20 due to complexities arising from electronelectron interactions [273].

Density functional theory (DFT), proposed by Hohenberg and Kohn building of the work of Thomas [274] and Fermi [275], is a reformulation of quantum mechanics in which, rather than the wavefunction, the ground state electron density n(r) becomes the fundamental parameter [276]. This allows an N-body problem to be constructed in terms of N single-body problems, in which every electron is treated as moving in a static external potential v(r). By solving the self-consistent Kohn-Sham equations (equations 7.2 – 7.4), one can find the ground state electron density for a system of non-interacting electrons in an external potential [277]:

$$\left[\frac{1}{2}\nabla_i^2 + v_{eff}(r)\right]\varphi_i(r) = \varepsilon_i\varphi_i(r)$$
(7.2)

$$n(r) = \sum_{i=1}^{N} |\varphi_i(r)|^2$$
(7.3)

$$V_{eff}(r) = V(r) + V_H(r) + V_{xc}(r)$$
(7.4)

where  $\nabla_i^2$  and V(r) are the same as those in the Schrodinger equation Hamiltonian,  $\varphi_i(r)$ are the single particle Kohn-Sham wave functions (analogous to  $\Psi$ ), V<sub>H</sub>(r) is the Hartree potential which describes the mean field potential of the electron density, and Vxc(r) is the local exchange-correlation potential which includes all exchange and correlation energies as well as any terms not accounted for by V(r) and V<sub>H</sub>(r).

In practice, DFT calculations proceed through an iterative approach:



#### 7.1 Computational Parameters

All DFT calculations were performed using The Vienna Ab initio Simulation Package (VASP) [278–281] on the Coeus compute cluster at Portland State University. VASP is primarily used for solid state DFT computations due to its use of the plane wave basis set, which takes advantage of the periodic structures of solids. For this work, exchange and correlation contributions were described by the generalized gradient approximation (GGA) with the Perdew-Burke-Ernzerhof (PBE) functional [282,283], while the atomic cores were represented by projector augmented wave (PAW) pseudopotentials [284,285]. In order to account for the strongly correlated d-electrons of the transition metals, a Hubbard potential (U) was applied through DFT+U [286,287]. U values in this work were determined by first optimizing U<sub>Ni</sub> and U<sub>Fe</sub> for nickel hexacyanoferrate, and then maintaining the same U<sub>Fe</sub> while determining U<sub>Mn</sub> in manganese hexacyanoferrate. The values for U are: U<sub>Ni</sub> = 5.3, U<sub>Mn</sub> = 4.3, and U<sub>Fe</sub> = 3.9.

Example INCAR, KPOINT, and POSCAR input files for a VASP calculation are provided in the Appendix. The INCAR file contains all of the input parameters for a calculation, telling VASP what to do. The KPOINT file determines the sampling of the Brillouin zone, and the POSCAR file contains information about the crystal structure. The other file that is require for a VASP calculation is the POTCAR file which contains the pseudopotentials and exchange-correlation functionals. All POTCAR files require a VASP license.

## 7.2 Initial results

DFT calculations were performed for Na<sub>2</sub>Ni[Fe(CN)<sub>6</sub>], Na<sub>2</sub>Mn<sub>25</sub>Ni<sub>75</sub>[Fe(CN)<sub>6</sub>], Na<sub>2</sub>Mn<sub>50</sub>Ni<sub>50</sub>[Fe(CN)<sub>6</sub>] and Na<sub>2</sub>MnHCF. For simplicity, Fe(CN)<sub>6</sub> vacancies, coordinated water and zeolitic water were not accounted for in the structures. The absence of these inputs was expected to cause some discrepancies between calculated and actual structures, however trends in calculated electron densities were expected to still be informative.

Prior to electronic structure calculations, the geometry and atom positions for each sample were optimized using VASP. Table 7.1 presents the calculated and experimentally determined lattice parameters for all materials. The DFT and X-ray diffraction results match well for the cubic samples, however the calculated MnHCF lattice is more distorted than the actual sample. The exaggerated distortion for the calculated MnHCF structure is attributed to the high Na content (full occupancy) and absence of interstitial water that were over-represented in the calculated structure; both of these factors are experimentally known to induce structural shifts [260,288].

Charge density plots for  $Na_2Ni[Fe(CN)_6]$  and  $Na_2Mn_{25}Ni_{75}[Fe(CN)_6]$  were produced to probe the effect that substitution of Mn for Ni has on the resulting material's electron distribution. Analysis of  $Na_2Mn[Fe(CN)_6]$  was not included because the effects of the monoclinic distortions on the electron density are unknown.

	Experimental	Calculated
$Na_2Ni[Fe(CN)_6]$	a=b=c = 10.21 Å	a=b=c = 10.13 Å
Na <sub>2</sub> Mn <sub>25</sub> Ni <sub>75</sub> [Fe(CN) <sub>6</sub> ]	a=b=c = 10.27 Å	a=b=c = 10.29 Å
Na2Mn50Ni50[Fe(CN)6]	a=b=c = 10.33 Å	a=b=c = 10.29 Å
Na <sub>2</sub> Mn[Fe(CN) <sub>6</sub> ]	a = 10.59 Å, b = 7.58 Å, c = 7.36 Å, β = 91.55°	a = 10.39 Å, b = 7.17 Å, c = 6.86 Å, β = 94.53°

 Table 7.1
 Experimental and theoretical lattice parameters for Na<sub>2</sub>Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>]

The charge density plots shown in Figure 7.1 and Figure 7.2. appear to support the hypotheses that the incorporation of Mn shifts the electron density towards the Fe-C end of the cyanide. For Na<sub>2</sub>Ni[Fe(CN)<sub>6</sub>], the charge density across every Ni-N-C-Fe chain is equivalent, a result of the symmetry of the material (Figure 7.1). Upon substitution of Mn, a clear break in the symmetry of the electron density is observed. Figure 7.2 displays the electron density plot for of Na<sub>2</sub>Mn<sub>25</sub>Ni<sub>75</sub>[Fe(CN)<sub>6</sub>] along the (200) plane, where two Ni and two Mn atoms are the nearest in-plane transition metals to the central Fe atom. Along the plane shown, there is a relative shift of charge density towards the Fe-C end of the cyanide in the Fe-CN-Mn chain compared to the Fe-CN-Ni chain. Additionally, the Fe-C bond length shortens from 1.893 Å for Fe-CN-Ni to 1.842 Å for Fe-CN-Mn, a contraction 140



**Figure 7.1** Charge density plot of Na<sub>2</sub>Ni[Fe(CN)<sub>6</sub>]

of 2.7%. In contrast, when the Fe atom is surrounded by 4 Ni-containing chains in the (010) plane, charge distribution between Fe and C is the again symmetric for all four carbons, as shown in Figure 7.3, similar to  $Na_2Ni[Fe(CN)_6]$ .

The initial density functional theory calculations appear to support the hypothesis, based on the experimental results, that substitution of Mn for Ni causes a shift in the



Figure 7.2 Charge density plot of Na<sub>2</sub>Mn<sub>0.25</sub>Ni<sub>0.75</sub>[Fe(CN)<sub>6</sub>] along the (200) plane

electron density towards the Fe-C end of the cyanide. This shift is highlighted by the Fe-C bond contraction along the Mn-N-C-Fe chain compared to the Ni-N-C-Fe chain in  $Na_2Mn_{0.25}Ni_{0.75}$ [Fe(CN)<sub>6</sub>]. Both of these results are consistent with the far IR absorption data presented in Figure 6.7.



Figure 7.3 Charge density plot of Na<sub>2</sub>Mn<sub>0.25</sub>Ni<sub>0.75</sub>[Fe(CN)<sub>6</sub>] along the (010) plane

#### Chapter 8.

#### Conclusion

## 8.1 Conclusions

The need for innovative and novel energy storage solutions has never been greater, with the impact of global warming becoming more evident by the day. Secondary batteries are bound to be part of a larger suite of storage technologies aimed at meeting global demands for generating electricity without producing greenhouse gases. Lithium ion batteries offer high energy densities and long lifetimes, which are necessary attributes for specific applications such as powering electric vehicles and portable electronics. However, for applications where energy and power density are not the most important factors, issues surrounding the limited supply of lithium salts, safety concerns, and inclusion of toxic materials start to overshadow the benefits of lithium batteries. In particular, there is a large and growing demand for safe and inexpensive mechanisms for storing electricity produced from non-CO<sub>2</sub> producing sources.

The work in this dissertation focused on the family of materials known as Prussian blue analogues (metal hexacyanometallates) as cathode materials for secondary battery systems. The overarching objectives were to:

1. Develop non-lithium ion based systems utilizing PBA cathodes, with a particular focus on divalent ion systems. Divalent ion batteries are of great interest as they

possess double the theoretical energy density compared to Li<sup>+</sup> for equal amounts of intercalated ions.

2. Determine if the electrochemical storage properties of two pure binary metal hexacyanoferrates could be improved by incorporating both metals into the metal hexacyanoferrate lattice. Of particular interest was what impacts Co or Ni would have on stabilizing manganese in the PBA lattice.

Chapter 3 presented the results of investigations into the use of Ca<sup>2+</sup> as the electrolyte in a battery system containing a Prussian blue (Fe<sup>3+</sup>[Fe<sup>2+</sup>(CN)<sub>6</sub>]) cathode and nonaqueous solvent (acetonitrile). This work demonstrated, for the first time, the suitability of Ca<sup>2+</sup> as a cation in a battery system consisting of a Fe[Fe(CN)<sub>6</sub>] cathode and acetonitrile solvent. With a specific capacity of 150 mAhg<sup>-1</sup>, this system delivered the highest reported specific capacity for any calcium ion battery using a Prussian Blue electrode. Calcium ion batteries are an intriguing alternative to lithium ion systems due to calcium's low cost, relative abundance (fifth most abundant element in the Earth's crust), and ability to offer double the energy density, per intercalated ion, of lithium ion batteries. By employing a nonaqueous chemistry, this work offers a proof of concept to future studies aimed at developing a CIB with a calcium metal anode.

The study presented in Chapter 4 demonstrated, for the first time, the use of Zn<sup>2+</sup> as a reversible intercalating cation with a manganese-cobalt hexacyanoferrate cathode in an aqueous solvent. Structure analysis of MnCoHCF0.50 coupled with energy

dispersive x-ray spectroscopy measurements confirmed a single phase with uniform distribution of Mn and Co throughout. A complex insertion/extraction process was highlighted by three distinct oxidation and reduction potentials. By combining manganese and cobalt the dissolution of Mn was prevented, while Mn redox provided a 21% increase (29 mAhg<sup>-1</sup>) in storage capacity compared to CoHCF. However, the mixed metal system suffered from increased capacity loss compared to CoHCF, 18% vs. 9% respectively, after the first 15 charge-discharge cycles. In general, aqueous zinc ion batteries offer high theoretical energy densities, as zinc is a divalent ion and Zn metal can be utilized as an anode. Additionally, the high safety profiles and low environmental impact of aqueous systems make them ideal to pair with solar and wind energy generation.

Chapter 5 presented an examination of the effects of coordinated and zeolitic H<sub>2</sub>O on the battery system consisting of a Cu[Fe(CN)<sub>6</sub>] cathode in a nonaqueous Mg<sup>2+</sup> electrolyte. Coordinated water was shown to play an important role in maximizing the specific capacity of the copper hexacyanoferrate in this system. Maintaining water within the CuHCF lattice resulted in a 25% increase in specific capacity when compared to the dehydrated sample. A nonaqueous electrolyte was chosen for this study because it is compatible with magnesium metal anodes metal, which could provide significant increases in energy density. In general, Mg metal is not volatile in air which reduces potential catastrophic failures, and Mg is relatively abundant (7th most abundant

element in the Earth's crust). In addition, difficulties in synthesizing a single phased mixed metal system containing manganese and copper were discussed.

Chapter 6 presented the use of Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>] as a cathode, with K<sup>+</sup> as the intercalating cation, in a non-aqueous solvent. The objective of this study was to determine if the introduction of both Ni and Mn into a mixed-metal hexacyanoferrate could provide improved capacity, compared to either NiHCF or MnHCF, by combining the crystal stability provided by Ni atoms with the favorable redox properties provided by Mn atoms.

Pure nickel hexacyanoferrate has the advantage of being structurally stable during discharge, but suffers from low specific capacity due to the redox inactivity of Ni. Pure manganese hexacyanoferrate has a high theoretical capacity, as Mn is redox active, however Jahn-Teller distortions during charging and discharging cause significant capacity loss over time [268].

Of the materials studied, Na<sub>2</sub>Mn<sub>0.50</sub>Ni<sub>0.50</sub>[Fe(CN)<sub>6</sub>] (MnNiHCF-2) delivered the highest specific capacity (110 mAhg<sup>-1</sup> at 25 mAg<sup>-1</sup>) without significant sacrifice in rate performance. This is attributed to the synergetic effects of manganese and nickel, with manganese providing addition storage capacity due to the Mn<sup>2+</sup>/Mn<sup>3+</sup> transition and nickel stabilizing the overall crystal structure and in particular the Fe-C-N-Mn chain. The addition of Mn increases the specific capacity of MnNiHCF-2 by 25% compared to pure

NiHCF. The stabilization offered by nickel enables fast K<sup>+</sup> diffusion and accounts for the good rate performance of MnNiHCF-2.

More broadly, a synergistic relationship between Mn and Ni in the mixed-metal hexacyanoferrate Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>] was demonstrated. An inverse relationship between rate capability and storage capacity was observed, with Mn<sub>50</sub>Ni<sub>50</sub>[Fe(CN)<sub>6</sub>] offering optimal pairing of storage capacity and diffusion kinetics. The combination of Mn and Ni offered increased capacities compared to NiHCF while only causing minimal loss with respect to rate performances. This result is consistent with the initial hypothesis that replacing Mn with Ni in the HCF lattice would improve electrochemical stability.

Chapter 7 presented the results of DFT calculations of electron charge density and changes in the iron-carbon bond lengths for the Na<sub>2</sub>Mn<sub>x</sub>Ni<sub>1-x</sub>[Fe(CN)<sub>6</sub>] materials studied in chapter 6. Initial results appear to support the hypothesis proposed after analysis of the experimental data . The charge density plots of Na<sub>2</sub>Ni[Fe(CN)<sub>6</sub>] and Na<sub>2</sub>Mn<sub>0.25</sub>Ni<sub>0.75</sub>[Fe(CN)<sub>6</sub>] demonstrate the polarization of the electron density away from the Mn atoms and towards the Fe-C bonds. Additionally, the optimized Na<sub>2</sub>Mn<sub>0.25</sub>Ni<sub>0.75</sub>[Fe(CN)<sub>6</sub>] structure revealed a 2.7% decrease in the Fe-C bond length for the Mn-N-C-Fe chain compared to the Ni-N-C-Fe chain. This finding further supports the conclusions drawn from the experimental FTIR data.

Collectively, the work presented in this dissertation provides novel insights into the applicability of Prussian blue analogues as cathode materials for non-lithium ion

batteries. PBAs are promising materials as they are generally inexpensive, easy to synthesize, and can accommodate a variety of intercalating ions. Additionally, the physical and electrochemical properties of a PBA can easily be tuned for specific applications by adjusting the transition metals in the host lattice, as was shown in chapters 4 and 6.

The four intercalating ions used in this dissertation were Ca<sup>2+</sup>, Zn<sup>2+</sup>, Mg<sup>2+</sup> and K<sup>+</sup>. Divalent ion systems, such as those in chapters 3, 4, and 5 are of great interest as they possess double the theoretical energy density compared to Li<sup>+</sup> for equal amounts of intercalated ions. Potassium ion batteries offer a high theoretical energy density resulting from the low reduction potential of potassium metal (-2.93 V verses standard hydrogen electrode), the low cost of potassium salts, and fast ionic mobilities.

### 8.2 Future work

The studies presented in this dissertation demonstrate progress towards the development of non-lithium ion batteries, and provide valuable insights into the relationships between the physical properties and storage capabilities of Prussian blue analogues. However, there is room to build on the work, focusing on three paths: continued exploration of the fundamental properties underlying the electrochemical and physical properties of mixed metal PBAs, addition of water to nonaqueous electrolytes, and application of the cathode materials presented in chapters 3-6 in a full battery.

Central to the studies of  $Mn_xCo_{x-1}[Fe(CN)_6]$  and  $Mn_xNi_{1-x}[Fe(CN)_6]$  was the ability to stabilize Mn in the PBA lattice by incorporating of a third transition metal. The resulting

mixed metal hexacyanoferrates delivered increased capacities compared to the binary parent Prussian blue analogues without significant negative consequences. To maximize the storage properties of both systems, other metal ratios should be synthesized to optimize the system. This will also provide insight into if there is a concentration of Mn where the Mn properties dominate and the mixed metal system becomes unstable. In addition to the two systems listed previously, Mn<sub>x</sub>Cu<sub>1-x</sub>[Fe(CN)<sub>6</sub>] synthesized using the hydrothermal synthesis discussed in section 5.1 offers a rout to study an unexplored mixed metal hexacyanoferrate system.

Pairing the future experimental work with further computational modeling would allow for a deeper understanding of the relationship between the specific metals in a mix metal hexacyanoferrate and the resulting materials properties. Some next steps should be vibrational mode analysis and electronic calculations using a hybrid functional. Vibrational mode analysis of the systems studied is necessary to better understand how the Ni/Mn ratio effects the bonding of the entire system. In addition to the cyanide bond, effects of Mn concentration on the nickel-nitrogen bond should be studied. Second, calculations using the hybrid functional HSE03 [289] could provide an accurate model for the electron density and properly describe the electronic properties of the materials.

Additionally, analysis of the "chemical bonding" of the PBAs should be conducted using the local-orbital basis suite towards electron-structure reconstruction (LOBSTER), which allows for the approximation of orbital-pair interactions to generate a "bondweighted" density of states. This provides information on bonding and antibonding states. Lastly, modeling of ionic diffusion pathways using the nudge elastic band method can provide important insight into the impact of Mn substitution on the migration of K<sup>+</sup> ions.

Building off of the work on hydrated copper hexacyanoferrate, it would be interesting to study the system in a hybrid aqueous/nonaqueous electrolyte. Hybrid electrolytes have started to gain interest in the battery community as a way to increase ionic mobility while maintaining a wide electrochemical potential window. This approach may lead to a system with good storage properties coupled with increased power density.

Finally, the development of full batteries, a two-terminal cell without a reference electrode, is an important next step. Of particular interest is the use of metallic anodes such as Zn, Ca, and Mg, which would provide significant increases in energy density. This would demonstrate the true applicability of the systems studied in this dissertation.

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# Appendices

## Appendix A: INCAR

For a full list of all INCAR parameters can be found at the VASP wiki [290].

ISTART = 0	# 0 for start, 1 for continuation				
ICHARG = 0	# 0 for start, 1 for continuation, 11 for DOS calculation				
ISPIN = 2	# Turns spin polarization calculations on				
NUPDOWN = 14 <i>#</i> Sets the difference between the number of electrons in the up and down spin components.					
MAGMOM = 4*0.0 48*0.0 8*.0 2*2.0 2*5.0 <i># Specifies the initial magnet moment for each atom</i>					
LASPH = .TRUE. <i>#Includes non-spherical contributions from the gradient corrections inside the PAW spheres</i>					
ISYM = 2	# Determines the way VASP treats symmetry				
# PBE + U calculation:					
LDAU = .TRUE. # Switch on LDA+U					
LDAUTYPE = 2 # LSDA + U Dudarev's approach = type 2 in vasp					
# Add on-site interaction for the respective atoms (same order as in POSCAR)					

*# Only the difference U-J is meaningful!!! U and J do not enter separately in the calculation.* 

LDAUL = 2 -1 -1 -1 2 2 # 2 for d-orbital interactions, -1 no on-site interaction

LDAUU = 3.9 0.0 0.0 0.0 5.3 4.3 # Define U-parameters for on-site Coulomb interaction

LDAUJ = 0.0 0.0 0.0 0.0 0.0 # Define J-parameters for on-site Exchange interaction

LDAUPRINT = 2 *# to print occupation matrix in OUTCAR* 

LMAXMIX = 4 *# in the case of LDA+U calculations LMAXMIX must be increased to 4 for d-electrons* 

# Accuracy:

ENCUT = 600	# energy cutoff for optimization
PREC = Accurate	# Specifies the "precision" mode
ADDGRID = .TRUE.	# Adds additional grid for evaluation of augmentation charges
ISMEAR = -5 # dete	rmines how the partial occupancies fnk are set for each orbital.
# 0 = q	aussian smearing, -5 = tetrahedron method with Blöchl corrections

#### *# electronic convergence*

EDIFF = 1E-6 *# maximal energy difference for stopping electronic relaxation* 

NELMDL = -5 # specifies the number of non-selfconsistent steps at the beginning. The negative number denotes the delay is only performed in the first ionic step

- NELMIN = 8 *# minimum number of electronic steps*
- NELM = 100 *# maximum number of electronic steps*

# ionic convergence

IBRION = 2 *# determines how the ions are updated and moved.* 

# 1 = quasi-newton algorithm, 2 = conjugate gradient algorithm, -1 = no update, used for non-self consistent and DOS calculations

EDIFFG = -0.001 *# defines the break condition for the ionic relaxation loop. If the change in the total (free) energy is smaller than EDIFFG between two ionic steps relaxation will be stopped.* 

NSW = 200 *#maximum number of ionic steps* 

ISIF = 3 *# Determines which degrees-of-freedom are allowed to change in relaxation.* 2 = *just position,* 3 = *position, cell shape, cell volume.* 

POTIM = 0.1 *# sets the step width scaling (ionic relaxations).* 

# For local charges and magnetization

LORBIT = 11 # gives magnetic moments and DOS

LAECHG = .TRUE. *# for Bader Charge analysis* 

LWAVE = .TRUE. *# write WAVECAR file* 

## **Appendix B: KPOINT**

The descriptions of each line in the following KPOINT file is reproduced from the VASP wiki [290]:

- 1: Header
- 2: Specifies the k mesh generation scheme. 0 denotes automatic
- 3: Specifies either Gamma-centered or Monkhorst-Pack grid
- 4: Number of subdivisions in each direction
- 5: Shift of the mesh

Auto 0 Monkhorst-Pack 8 8 8 0.0 0.0 0.0 The descriptions of each line in the following POSCAR file is reproduced from the VASP wiki [290]:

- 1: Header or comments
- 2: overall scaling constant
- 3-5: Bravis matrix
- 6: Name(s) of atom(s)
- 7: Number of the atoms (of each atom type)
- 8: Specifies which coordinate system is used ("cartesian" or "direct")
- 9 end: Positions of atoms

## NiHCF

1.0							
1	0.2	2000	000	000	0.0000000000		0.0000000000
(	0.0000000000				10.2200000000		0.0000000000
(	0.00	000	000	00	0.00000000	00	10.2200000000
Fe	Ν	С	Κ	Ni			
4	24	24	8	4			
Direc	t						
0.0	000	0000	000		0.500000000	0.0	00000000
0.0	000	0000	000		0.000000000	0.5	50000000
0.	500	0000	000		0.000000000	0.0	00000000
0.50000000					0.500000000	0.5	50000000
0.200900641				0.000000000	0.0	00000000	
0.	0.799099359				0.000000000	0.0	00000000
0.000000000					0.200900641	0.0	00000000
0.000000000					0.799099359	0.0	00000000
0.000000000					0.000000000	0.2	200900641
0.0	0.000000000				0.000000000	0.7	99099359
0.2	0.200900641				0.500000000	0.5	50000000
0.	0.799099359				0.500000000	0.5	50000000
0.0	0.00000000				0.700900594	0.5	50000000
0.0	0.000000000				0.299099359	0.5	50000000
0.0	0.000000000				0.500000000	0.7	00900594
0.0	0.000000000				0.500000000	0.2	99099359
0.	0.700900594				0.000000000	0.5	50000000

0.299099359	0.000000000	0.500000000
0.500000000	0.200900641	0.500000000
0.500000000	0.799099359	0.500000000
0.500000000	0.000000000	0.700900594
0.500000000	0.000000000	0.299099359
0.700900594	0.500000000	0.000000000
0.299099359	0.500000000	0.000000000
0.500000000	0.700900594	0.000000000
0.500000000	0.299099359	0.000000000
0.500000000	0.500000000	0.200900641
0.50000000	0.500000000	0.799099359
0.316067871	0.000000000	0.000000000
0.683932106	0.000000000	0.000000000
0.000000000	0.316067871	0.000000000
0.000000000	0.683932106	0.000000000
0.000000000	0.000000000	0.316067871
0.000000000	0.000000000	0.683932106
0.316067871	0.500000000	0.500000000
0.683932106	0.500000000	0.500000000
-0.00000000	0.816067894	0.50000000
0.000000000	0.183932129	0.50000000
-0.00000000	0.500000000	0.816067894
0.000000000	0.50000000	0.183932129
0.816067894	0.000000000	0.50000000
0.183932129	0.000000000	0.50000000
0.50000000	0.316067871	0.50000000
0.50000000	0.683932106	0.50000000
0.50000000	-0.000000000	0.816067894
0.50000000	0.000000000	0.183932129
0.816067894	0.50000000	0.000000000
0.183932129	0.50000000	0.000000000
0.50000000	0.816067894	0.000000000
0.50000000	0.183932129	0.000000000
0.50000000	0.50000000	0.316067871
0.50000000	0.50000000	0.683932106
0.750000000	0.750000000	0.750000000
0.250000000	0.250000000	0.750000000
0.250000000	0.750000000	0.250000000
0.750000000	0.250000000	0.250000000
0.750000000	0.750000000	0.250000000
0.750000000	0.250000000	0.750000000
0.25000000	0.750000000	0.750000000

0.250000000	0.250000000	0.250000000
0.000000000	0.000000000	0.00000000
0.000000000	0.500000000	0.50000000
0.500000000	0.000000000	0.50000000
0.500000000	0.500000000	0.00000000